Article

# Active species in chloroaluminate ionic liquids catalyzing low-temperature polyolefin deconstruction

Received: 26 January 2024

Accepted: 18 June 2024

Published online: 10 July 2024

Check for updates

Wei Zhang <sup>1,2</sup> , Rachit Khare<sup>2</sup>, Sungmin Kim <sup>1</sup>, Lillian Hale<sup>1</sup>, Wenda Hu<sup>1</sup>, Chunlin Yuan<sup>2</sup>, Yaoci Sheng<sup>2</sup>, Peiran Zhang <sup>2</sup>, Lennart Wahl<sup>2</sup>, Jiande Mai<sup>1</sup>, Boda Yang<sup>1</sup>, Oliver Y. Gutiérrez <sup>1</sup>, Debmalya Ray<sup>1</sup>, John Fulton<sup>1</sup>, Donald M. Camaioni <sup>1</sup>, Jianzhi Hu <sup>1,3</sup>, Huamin Wang<sup>1</sup>, Mal-Soon Lee <sup>1</sup> & Johannes A. Lercher <sup>1,2</sup>

Chloroaluminate ionic liquids selectively transform (waste) polyolefins into gasoline-range alkanes through tandem cracking-alkylation at temperatures below 100 °C. Further improvement of this process necessitates a deep understanding of the nature of the catalytically active species and the correlated performance in the catalyzing critical reactions for the tandem polyolefin deconstruction with isoalkanes at low temperatures. Here, we address this requirement by determining the nuclearity of the chloroaluminate ions and their interactions with reaction intermediates, combining in situ<sup>27</sup>Al magicangle spinning nuclear magnetic resonance spectroscopy, in situ Raman spectroscopy, Al K-edge X-ray absorption near edge structure spectroscopy, and catalytic activity measurement. Cracking and alkylation are facilitated by carbenium ions initiated by AlCl<sub>3</sub>-tert-butyl chloride (TBC) adducts, which are formed by the dissociation of  $Al_2Cl_7^-$  in the presence of TBC. The carbenium ions activate the alkane polymer strands and advance the alkylation cycle through multiple hydride transfer reactions. In situ <sup>1</sup>H NMR and operando infrared spectroscopy demonstrate that the cracking and alkylation processes occur synchronously; alkenes formed during cracking are rapidly incorporated into the carbenium ion-mediated alkylation cycle. The conclusions are further supported by ab initio molecular dynamics simulations coupled with an enhanced sampling method, and model experiments using n-hexadecane as a feed.

Upcycling discarded polyolefins into a range of products that align with existing end markets is a critical step towards achieving a circular economy<sup>1,2</sup>. Polyolefin waste could be a promising feedstock for a next-generation refinery, with volumes (~160 Mt/yr<sup>-1</sup>; 2019) equivalent to 1 billion barrels of crude oil refining capacity<sup>3,4</sup>.

Current catalytic technologies to convert spent polyolefins into transportation fuels rely on catalytic pyrolysis and hydrocracking over solid acid catalysts, for which significant energy input at high temperatures (T > 300 °C) is required to overcome the endothermic C-C cleavage<sup>5-7</sup>. To overcome thermodynamic limitations, recent

<sup>&</sup>lt;sup>1</sup>Institute for Integrated Catalysis, Pacific Northwest National Laboratory, P.O. Box 999, Richland WA, USA. <sup>2</sup>Department of Chemistry and Catalysis Research Center, Technische Universität München, Lichtenbergstr. 4, Garching, Germany. <sup>3</sup>The Gene and Linda Voiland School of Chemical Engineering and Bioengineering, Washington State University, Pullman, WA, USA. e-mail: wzhangx@outlook.com; johannes.lercher@ch.tum.de



**Fig. 1** | **Tandem cracking-alkylation for converting polyolefins to liquid alkanes with chloroaluminate ionic liquids.** Schematic illustration of the endothermic C-C bond cleavage of polyolefins, kinetically coupled with the exothermic alkylation of the resulting olefin intermediate, enabling low-temperature conversion of polyolefins into liquid alkanes in ionic environments.

approaches utilize hydrocracking or hydrogenolysis<sup>8-13</sup>, tandem hydrogenolysis-aromatization<sup>14</sup>, dehydrogenation-metathesis<sup>15-18</sup>. These methods achieve conversions beyond the equilibrium conversion for cracking at low temperatures. However, these tandem processes still require moderate to high reaction temperatures (~200–250 °C) and suffer from severe catalyst deactivation by coking<sup>19,20</sup>.

Recently, we reported a low-temperature strategy for upgrading discarded polyolefins to gasoline-range iso-alkanes in a single-stage process catalyzed by an acidic chloroaluminate-based ionic liquid (Fig. 1)<sup>21</sup>. This approach kinetically couples the endothermic cleavage of the polymer C–C bonds with the exothermic alkylation of iso-paraffins, hence, thermodynamically allowing full conversion of the polymer below 100 °C. However, the identification of the active catalyst speciation in this complex transformation has remained unresolved. It should be noted that this represents a longstanding question in the study of chloroaluminate-based ionic liquids for reaction such as paraffin alkylation, despite the extensive research and the well-established industrial application<sup>22,23</sup>.

Chloroaluminate ionic liquids mainly consist of  $AlCl_4^-$  and  $Al_2Cl_7^$ anions. The mononuclear  $AlCl_4^-$  is chemically relatively inert<sup>24</sup>. Consequently, its adduct with  $AlCl_3$ , i.e.,  $Al_2Cl_7^-$  has been suggested to be the catalytically active site<sup>25</sup>. However, our preceding kinetic analysis showed that the initial low-density polyethylene (LDPE) conversion rate was not proportional to the concentration of  $Al_2Cl_7^-$ . We then hypothesize that a small concentration of  $AlCl_3$  from the dissociation of  $Al_2Cl_7^-$  (Supplementary Fig. 1) functions as an ephemeral transition structure<sup>21</sup>. This monomeric  $AlCl_3$  can not be detected analytically, but its concentration can be derived via the equilibrium constants as it is in equilibrium with  $AlCl_4^-$  and  $Al_2Cl_7^-$ . Additionally, alkyl chloride additives are essential in chloroaluminate-based ionic liquid-catalyzed alkylation of isoparaffins with olefins. Numerous studies have attributed the effectiveness of these additives to the in-situ generation of  $HCl^{26}$ , functioning similarly to classical Brønsted acid-catalyzed alkylation processes, such as those involving hydrofluoric acid (HF) or sulfuric acid (H<sub>2</sub>SO<sub>4</sub>)<sup>27</sup>. Jess and coworker showed that halide additives are the carbenium ion initiators that directly generate the carbenium ions for the alkylation reaction, in contrast to Brønsted-acid, where this species is indirectly formed through a hydride shift between protonated butene and isobutane<sup>28</sup>. The challenge lies in elucidating the dual roles of chloroaluminate ions, especially speculative monomeric AlCl<sub>3</sub>, and the alkyl chloride additive, in the carbenium ion-based mechanism that drives the interconnected cracking and alkylation cycles.

In this study, we address questions concerning the speciation of chloroaluminate species and their role in the low-temperature activation and subsequent tandem cracking-alkylation for polyolefin conversion in the presence of iso-paraffins. We elucidate the nature and structural dynamics of chloroaluminate species within ionic liquids, employing a combination of <sup>27</sup>Al magic-angle spinning nuclear magnetic resonance spectroscopy (27Al MAS NMR), in situ Raman spectroscopy, and Al K-edge X-ray absorption near edge structure spectroscopy. It is shown that the reaction is started by small amounts of TBC reacting with in situ generated AlCl<sub>3</sub> by dissociation of Al<sub>2</sub>Cl<sub>7</sub>, providing the initial carbenium ions for the chain process. It should be emphasized that the carbenium ions remain always associated with the formed AlCl4- anions. The initial tert-butyl carbenium ions activate the C-H bonds of alkanes (LDPE and iC<sub>5</sub>) via hydride transfer. Kinetic control experiments, along with the atomistic simulations, using linear hexadecane (n-C<sub>16</sub>) as probe molecules are used to elucidate the reaction mechanisms.

#### Results

#### Synthesis and characterization of ionic liquids

We first identify the structure of the chloroaluminate species and establish qualitative methods to monitor them under operation conditions. Chloroaluminate ionic liquids were prepared by mixing anhydrous AlCl<sub>3</sub> with N-butyl pyridinium chloride at various ratios. The samples are denoted as [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub>, wherein x represents the molar ratio of AlCl<sub>3</sub> and [C<sub>4</sub>Py]Cl (see the experimental section for details). The structure of chloroaluminate species is determined by Al K-edge X-ray absorption near edge structure (XANES) and k<sup>2</sup>weighted Fourier-transformed extended X-ray absorption fine structure (FT-EXAFS) of [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> ionic liquids with varying [C<sub>4</sub>Py]Cl:AlCl<sub>3</sub> molar ratios (Supplementary Fig. 2). The chloroaluminate speciation of [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> comprises monomeric AlCl<sub>4</sub><sup>-</sup> and dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> anions. In the monomeric AlCl<sub>4</sub><sup>-</sup> species, the Al atom is symmetrically coordinated to four chloride ions with identical Al–Cl bond lengths (~2.16 Å). In the dimeric Al<sub>2</sub>Cl<sub>7</sub>, the coordination structure around Al is asymmetric. The Al-Cl bond length for the six terminal chloride ions is ~2.12 Å, whereas for the bridging chloride ion (Clbridge), it is ~2.29 Å, indicating distorted tetrahedral symmetry. More details can be found in supplementary note 1, including the systematic increase in the Debye-Waller factor through EXAFS fitting analysis (see Supplementary Figs. 3-6 and Supplementary Table 1).

The chloroaluminate species in the ionic liquids were further identified using <sup>27</sup>Al MAS NMR spectroscopy (Fig. 2a). The spectrum for x = 1 ([C4Py]Cl:1AlCl<sub>3</sub>) only showed a sharp signal at ~103 ppm, which is assigned to monomeric AlCl<sub>4</sub><sup>-29</sup> Increasing the fraction of anhydrous AlCl<sub>3</sub> (x > 1) broadens the resonance signal, accompanied by a new peak at ca. 97 ppm. This peak is attributed to the formation of dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> in equilibrium with AlCl<sub>4</sub><sup>-30</sup>. The increase of the mole ratio to 2.5 ([C4Py]Cl:2.5AlCl<sub>3</sub>) led to a signal for solid aluminum chloride (~0 ppm). We hereby focus on the homogenous [C<sub>4</sub>Py]Cl-AlCl<sub>3</sub> ionic liquids, with a mole ratio below 2.5, for catalysis in which monomeric AlCl<sub>4</sub><sup>-</sup> and dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> dominate.



**Fig. 2** | **27AI MAS NMR and Raman spectroscopy on chloroaluminate ionic liquids. a** <sup>27</sup>AI MAS NMR spectra of [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> (x = 1-2.5). b Integrated FWHM of <sup>27</sup>AI resonances as a function of temperatures over [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub>. **c** Integrated FWHM of <sup>27</sup>AI resonances as a function of mole ratio of AlCl<sub>3</sub>/[C<sub>4</sub>Py]Cl (x) at different temperatures. **d** DFT-simulated Raman spectra of AlCl<sub>4</sub><sup>-</sup>, Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>, and DCM.

**e** Plot of the Raman area ratio of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> versus the molar ratio of AlCl<sub>3</sub>/ [C<sub>4</sub>Py]Cl (x); (Note that the area ratio of Raman signals at 310 cm<sup>-1</sup> and 350 cm<sup>-1</sup> depends closely on the molar ratio of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> and AlC<sub>4</sub><sup>-</sup>, respectively, derived from the Raman spectra in Supplementary Fig. 9). **f** Relationship between integrated FWHM of <sup>27</sup>Al resonances and the Raman area ratio of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> at 30 °C.

We further performed <sup>27</sup>Al NMR at varying temperatures from 30 °C to 80 °C for identify the chloroaluminate species. As shown in Supplementary Fig. 7a, the sharp signal of [C<sub>4</sub>Py]Cl-1AlCl<sub>3</sub> was consistent at different temperatures, indicating that the mononuclear AlCl<sub>4</sub><sup>-</sup> species are chemically inert. In the case of ionic liquids with an excess of anhydrous AlCl<sub>3</sub> to  $[C_4Py]Cl$  (x > 1, Supplementary Fig. 7, b-f), the two peaks at 103 and 97 ppm broadened with increasing aluminum content without a significant chemical shift. Numerous studies directly assigned the resonances at 103 and 97 ppm to AlCl<sub>4</sub><sup>-</sup> and  $Al_2Cl_7$  respectively<sup>31-34</sup>. However, the two individual signals cannot be directly related to the concentrations of  $Al_2Cl_7$  and AlCl<sub>4</sub><sup>-35</sup>. A dynamic interconversion between Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> and AlCl<sub>4</sub><sup>-</sup> broadens linewidths, contributing to the resonance assigned to AlCl<sub>4</sub><sup>-</sup> at around 103 ppm<sup>36</sup>. This is supported by DFT-NMR calculations (Supplementary Fig. 8a and b). The integrated line widths quantified by the full width at half maximum (FWHM) as a function of temperatures directly reflected this trend (Supplementary Fig. 8c)<sup>37</sup>. Fig. 2b shows that the two resonances at 103 and 97 ppm gradually narrowed with increasing temperature. The integrated FWHM of <sup>27</sup>Al resonances increased linearly with the molar ratio of  $AlCl_3/[C_4Py]Cl$ with good correlations ( $R^2 > 0.98$ ) among all spectra with varying temperatures (Fig. 2c). We infer that increasing temperature intensified the rate of molecular motions and the interconversion between  $Al_2Cl_7$  and  $AlCl_4$ , thereby exhibiting better-defined resonance signals<sup>38,39</sup>.

The Raman spectra of the  $[C_4Py]Cl-xAlCl_3$  ionic liquids (Fig. 2d and Supplementary Fig. 9) show a characteristic peak at 350 cm<sup>-1</sup>, which is attributed to the symmetric Cl–Al–Cl stretch of AlCl<sub>4</sub><sup>-</sup> anions<sup>40</sup>. The intensity of the AlCl<sub>4</sub><sup>-</sup> peak decreased gradually with increasing concentrations of anhydrous AlCl<sub>3</sub>, accompanied by the increase of the peaks at 310 cm<sup>-1</sup> and 430 cm<sup>-1</sup> that are assigned to the symmetric Al–Cl–Al and terminal Al–Cl stretching of dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> anions, respectively<sup>41</sup>. The observation suggests that anhydrous AlCl<sub>3</sub> drives the transformation from AlCl<sub>4</sub><sup>-</sup> and Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>. The ratio of the areas of the signals at 310 cm<sup>-1</sup> and 350 cm<sup>-1</sup> (Fig. 2e) mirrors the molar ratio of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> to AlCl<sub>4</sub><sup>-41-43</sup>. The FWHM of <sup>27</sup>Al resonances against area ratios (Fig. 2f) showed a linear correlation (R<sup>2</sup> = 0.991).

The combination of in situ <sup>27</sup>Al MAS NMR and Raman spectroscopy establishes, therefore, a quantitative relation of the formation of monomer and dimer aluminate species in ionic liquids that enables also monitoring the species under operation conditions. The changes in concentrations of AlCl<sub>4</sub><sup>-</sup> and Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> (Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> AlCl<sub>4</sub><sup>-</sup> + AlCl<sub>3</sub>) over various time intervals (t) simplified as  $\sum [AlCl_3]_t = \Delta [AlCl_4]_t$ , and the Al mole fraction ( $\chi_{Al}$ ) of chloroaluminate species can be expressed as Equations (Eqs. 1–2) (see detailed derivations in Supplementary Note 2):

$$\chi_{Al} \left( \sum [AlCl_3] \right)_t = \chi_{Al} \left( AlCl_4^{-} \right)_t = \frac{1}{2 \left( \frac{Area_{310cm^{-1}}}{Area_{350cm^{-1}}} \right)_t} + 2$$
(1)



Fig. 3 | In situ <sup>27</sup>Al MAS NMR on [C4Py]Cl-2AlCl3 catalyzed LDPE deconstruction. a Recorded of [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub> reacting with TBC with varying [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub> /TBC ratio from 0 to 1. **b** The computational simulations of Al<sub>2</sub>Cl<sub>7</sub>-reacting with TBC to form AlCl<sub>3</sub>-TBC adduct. The standard Helmholtz free energies ( $\Delta$ F°), dependent on the Al–Cl distance (R<sub>Al–Cl</sub>) between two molecules, are accompanied by atomic configurations that depict the initial, transition, and intermediate states. These data

were derived through ab initio molecular dynamics simulations in conjunction with the Blue Moon ensemble method. **c** Recorded during temperature-programmed reaction of LDPE over  $[C_4Py]Cl-2AlCl_3$  from room temperature (r.t.) to 100 °C; **d** Recorded by adding TBC to the  $[C_4Py]Cl-2AlCl_3$  catalyzed LDPE reaction at room temperature and 60 °C, respectively.

$$\chi_{Al} (Al_2 Cl_7^{-})_t = 1 - \frac{1}{\left(\frac{Area_{310cm^{-1}}}{Area_{350cm^{-1}}}\right)_t} + 1}$$
(2)

#### Variation of the chloroaluminate species during the reaction

In situ <sup>27</sup>Al NMR experiments were then used to monitor the restructuring of the chloroaluminate species during the reaction. Previous experiments showed that the significant enhancement in LDPE conversion observed with TBC addition<sup>21</sup>. We now probe the interaction of the chloroaluminate species with TBC, the carbenium ion initiator<sup>28</sup>, and reaction intermediates during LDPE conversion. Figure 3a shows that the addition of TBC decreased the linewidth of Al signals. This indicates that  $Al_2Cl_7^-$  and TBC react, forming a more symmetric species by chloride abstraction. Although the linewidths of Al decreased upon the addition of a molar aliquot of TBC compared to when it constituted only one-third, the reduction was not significant. This suggests that the equilibrium is shifted toward the more symmetric species as the relative concentration of TBC increases.

Utilizing ab initio molecular dynamics (AIMD) simulations coupled with a Blue Moon ensemble method (Fig. 3b), we found that the reaction between Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> and TBC to yield AlCl<sub>4</sub><sup>-</sup> and the AlCl<sub>3</sub>-TBC adduct (Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> + TBC  $\rightleftharpoons$  AlCl<sub>4</sub><sup>-</sup> + AlCl<sub>3</sub>...TBC) had a significantly lower energy barrier of 37 kJ/mol compared to direct Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> dissociation (Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>  $\rightleftharpoons$  AlCl<sub>4</sub><sup>-</sup> + AlCl<sub>3</sub>), which exhibits a higher activation energy of 59 kJ/mol (Supplementary Fig. 10). The absence of detected adducts is attributed to interference from the multinuclearity of chloroaluminate anions in chloroaluminate ionic liquids, as the formation of monomeric AlCl<sub>3</sub> adducts, typically detectable at ~99 ppm<sup>44,45</sup>.

Figure 3c shows the temperature-programmed in situ <sup>27</sup>Al MAS NMR of  $[C_4Py]Cl-2AlCl_3$  in the presence of LDPE, compared with pure ionic liquids. Upon adding LDPE, the Al resonances at 103 and 97 ppm were well preserved and slightly narrowed with increasing temperatures. This observation suggests that the direct deconstruction of LDPE is limited due to endothermic C-C cleavage. Further adding TBC



Fig. 4 | In situ Raman spectra on [C4Py]CI-2AlCl3 reacting with LDPE and n-hexadecane as a model reactant. a In situ Raman spectra recorded during the cracking-alkylation of LDPE and iC<sub>5</sub> in the presence of TBC additive. **b** The timeresolved conversion profile of LDPE and the corresponding variation of chloroaluminate species using Equation (Eq. (1)). **c** The n-C<sub>16</sub> consumption as a function of chloroaluminate species in consecutive processes. **d** the initial rate (calculated as grams of LDPE converted per minute) as a function of Al-adducts concentration. Note: we studied the rates at low conversions <20 wt. %. The changes in concentrations over various time intervals are expressed as  $\sum[Al-adduct] = \Delta[AlCl_4-]$ . Conditions: a-b: LDPE, 200 mg; iC<sub>5</sub>, 800 mg; [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>, 2 mmol; TBC, 5 mg;

DCM, 3 ml; and temperature, 70 °C. c: In the 1<sup>st</sup> run, 150 mg of n-C<sub>16</sub>, 600 mg of iC<sub>5</sub> and 5 mg of TBC as an additive were added into the reactor containing 2 mmol of [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub> and 3 ml of DCM. Upon n-C<sub>16</sub> was fully converted, the reactor was rapidly cooled under -30 °C and replenish with another 150 mg of fresh n-C<sub>16</sub>. **e**-**f** The standard Helmholtz free energy ( $\Delta$ F°) of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> catalyzed hydride abstraction from iC<sub>5</sub> (**e**) and AlCl<sub>3</sub>-TBC adduct catalyzed hydride abstraction from n-C<sub>16</sub> (**f**) as a function of the molecular distance between reacting molecules, achieving via ab initio molecular dynamics simulations coupled with a Blue Moon ensemble method.

as a co-reagent with LDPE significantly narrowed the Al resonances, which points to a significant depletion of  $Al_2Cl_7$  species (Fig. 3d). This observation is further supported by a series of spectra obtained at 60 °C.

Therefore, we deduced that the reaction is initiated by TBC reacting with AlCl<sub>3</sub> that is in situ generated from the dissociation of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>, forming the AlCl<sub>3</sub>-TBC adduct (AlCl<sub>3</sub>···Cl···iC<sub>4</sub>). The adducts readily undergo a transformation into reactive ion-pair species (i.e., carbenium ions and AlCl<sub>4</sub><sup>-</sup>), activating the reacting molecules via consecutive hydride transfer and facilitating the propagation of carbenium ions. Notably, the formed carbenium ions are not bare cations but are surrounded and stabilized by the counterpart AlCl<sub>4</sub><sup>-</sup> anions, existing in the form of stable ion pairs<sup>46</sup>. This can explain why the initial reaction rate is directly correlated with the concentration of TBC loading and dissociation of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> (Supplementary Fig. 11).

The dynamic transformation of these chloroaluminate species within ionic liquids can also be monitored through in situ Raman spectroscopy throughout the reaction. The Raman spectra of  $[C_4Py]Cl$ -xAlCl<sub>3</sub> in the presence and absence of TBC were nearly identical (Supplementary Fig. 12). This further implies that the resulting Al species predominantly exist as organic adducts. Otherwise, the presence of AlCl<sub>4</sub><sup>-</sup> (along with carbenium ions) would be reflected by a distinct Raman signal specific to AlCl<sub>4</sub><sup>-</sup>.

Then, we conducted time-resolved in situ Raman spectroscopy of  $[C_4Py]Cl-2AlCl_3$  in the presence of LDPE and  $iC_5$  together with TBC additive at 70 °C (Fig. 4a). The characteristic band of  $Al_2Cl_7^-$  at 310 cm<sup>-1</sup> gradually weakens with reaction time, accompanied by an increase in the new characteristic band of  $AlCl_4^-$  (350 cm<sup>-1</sup>). These variations in  $Al_2Cl_7^-$  and  $AlCl_4^-$  concentration are used to quantitatively evaluate the

concentration of formed AlCl<sub>3</sub> (which exists as an adduct). Clearly, the variation of x(Al) of chloroaluminate species showed a close correlation with LDPE conversion (Fig. 4b). Initially, the Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> species was rapidly consumed, and its fraction decreased by ~0.3 when 40% of LDPE was converted. The remaining LDPE (60%) only consumed ~0.1 of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> (Supplementary Fig. 13). This was also observed with the variation of  $Al_2Cl_7^-$  and  $AlCl_4^-$  using n-C<sub>16</sub> as a reactant instead of LDPE (Supplementary Fig. 14). Particularly in consecutive runs, the chloroaluminate components were kept constant during the conversion of  $n-C_{16}$  (Fig. 4c). This stabilization is attributed to the generation of catalytically active species originating from the dissociation of Al<sub>2</sub>Cl<sub>7</sub>during the initial stages of the reaction, which then rapidly reaches equilibrium. This process enables the propagation of carbenium ions through consecutive hydride transfers between LDPE and iC<sub>5</sub>. We found that the initial reaction rate is proportional to the concentration of  $\Sigma$ [Al-adduct] (Fig. 4d), suggesting AlCl<sub>3</sub>-complex formed in situ through the dissociation of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> functions as the catalyst.

The AIMD simulations revealed that the hydride transfer between  $Al_2Cl_7^-$  and hydrocarbons (e.g.,  $iC_5$ ) is a strongly endothermic process, continuously increasing up to 147 kJ/mol (Fig. 4e and Supplementary Fig. 15). This suggests that the  $Al_2Cl_7^-$  species is not a catalytically active species and, therefore, is hypothesized not to catalyze the hydride transfer. In contrast, the hydride transfer from n-C<sub>16</sub> to the AlCl<sub>3</sub>-TBC complex is only 17 kJ/mol (Fig. 4f and Supplementary Fig. 16). The  $iC_4^+$  formed from TBC can easily attract/accept a hydride of the PE chain, resulting in the formation of  $iC_4$  and PE<sup>+</sup>-AlCl<sub>4</sub><sup>-</sup> adducts (AlCl<sub>3</sub>-..Cl...PE). In the transition state (TS), the proximity of PE to the AlCl<sub>3</sub>-TBC complex leads to the interaction between PE and  $iC_4^+$  and the formation of AlCl<sub>4</sub><sup>-</sup> with an activation energy of 30 kJ/mol. These simulation



Fig. 5 | Following the deconstruction of LDPE Operando IR study of conversion over ionic liquids. Operando IR spectra recorded in the presence of  $iC_5$  over  $[C_4Py]$  Cl-2AlCl<sub>3</sub>. Conditions: LDPE, 2 g;  $iC_5$ , 8 g; DCM, 30 ml;  $[C_4Py]$ Cl-2AlCl<sub>3</sub>, 20 mmol; TBC 0.5 mmol, and temperature, 60 °C. Data were acquired with an automatic sample scan interval of 15 s over the range of 4000-700 cm<sup>-1</sup>.

results agree well with the in situ NMR and Raman spectroscopy, which indicate that the AlCl<sub>3</sub>-TBC adduct (AlCl<sub>3</sub>····Cl···iC<sub>4</sub>) acts as an active species. It induces intramolecular hydride transfer at the initial stage, providing the initial carbenium ions necessary to start the reaction.

## Mechanism and kinetics of catalytic deconstruction of LDPE via tandem cracking-alkylation

It is important to note that alkenes are hardly observed in the product stream; only trace amounts of propene (less than 0.1 wt. %) were observed in the headspace during the cracking-alkylation of LDPE and  $iC_5$ . We inferred that cracking and alkylation are kinetically coupled and proceed, thus, with identical rates. The activated hydrocarbon strands of polymers will crack at positions determined by the rates of hydride shift within the chain. Increasing the hydride shift rate compared to cracking will, thus, lead to longer cracked fragments and heavier products; on the contrary, the relatively higher rate of cracking will give more alkenes, facilitating the formation of acid-soluble oil via oligomerization (as the alkylation is a significantly slower reaction than the oligomerization of the alkenes).

To monitor alkene formation, we employed in situ <sup>1</sup>H NMR spectroscopy for tandem-cracking-alkylation, using n-C<sub>16</sub> as a model reactant with iC<sub>5</sub> in the presence of TBC additive over [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub> (Supplementary Fig. 17). We found that the variation of unsaturated hydrogen atoms within the olefinic region (4.4-6.5 ppm) indicates the presence and fluctuation of olefinic intermediates during the reaction. The ratio of unsaturated chains remains constant, maintaining a low concentration of ~0.2-0.5% throughout the reaction. To further explore the impact of olefins on the tandem cracking-alkylation of LDPE and iC<sub>5</sub>, isopentene ( $C_5^{=}$ ) was introduced instead of the TBC additive (Supplementary Fig. 18). However, this resulted in only 18 wt.% conversion to LDPE, showing no noticeable improvement compared to baseline conditions lacking such additives (Supplementary Fig. 19). Our AIMD-based Blue Moon ensemble simulation confirmed this by showing a highly endothermic process ( $\Delta F^{\circ} = 125 \text{ kJ/mol}$ ) responsible for forming the AlCl<sub>4</sub><sup>-</sup> and AlCl<sub>3</sub>-C<sub>5</sub><sup>-</sup> adduct through interaction between  $Al_2Cl_7^-$  and  $C_5^=$  (see Supplementary Fig. 20).

Obviously,  $C_5^{=}$  exhibits a pronounced preference for oligomerization over alkylation, which is in agreement with chloroaluminate ionic liquid-catalyzed olefin oligomerization<sup>28</sup>. Thus, we conclude that alkenes, generated synchronously during the cracking cycle, engage in very rapid alkylation reactions with iC<sub>5</sub>. This interaction significantly alters the equilibrium via the exothermic alkylation of alkene fragments, thus, effectively suppressing olefin oligomerization.

For real-time monitoring of these reactions, we then employed operando infrared spectroscopy, which provided insights into the transformations occurring within the LDPE substrate during the reaction (Supplementary Fig. 21). The time-resolved IR spectra of LDPE in the presence of ionic liquids at 60 °C displayed characteristic LDPE bands (Supplementary Fig. 22). The sp<sup>3</sup> C-H vibrations at 2913 cm<sup>-1</sup> and 2845 cm<sup>-1</sup>, attributed to  $v_{as}(CH_2)$  and  $v_s(CH_2)$  of LDPE chains<sup>47</sup>, respectively, increased in intensity with time (Supplementary Fig. 22 a and b). This increase indicates that more of the polyolefin was observable at the monitoring window of the reaction cell, i.e., the spectroscopically accessible volume increased. Notably, the appearance of weak signals corresponding to terminal CH<sub>3</sub> groups indicates the limited LDPE deconstruction, attributable to the endothermic cleavage of the C-C bonds, which is thermodynamically unfavorable at such low temperatures. This observation is corroborated by in situ <sup>27</sup>Al NMR spectra recorded for LDPE deconstruction (Supplementary Fig. 22c), reinforcing the conclusion regarding the restricted deconstruction of LDPE in the absence of  $iC_5$ .

Subsequently, we employed this approach with LDPE and  $iC_5$ under otherwise identical conditions to follow the transformations (Fig. 5). Initially, new vibrations are assigned exclusively to  $iC_5$ , whose main characteristics are the  $v_{as}(CH_3)$  and  $v_s(CH_3)$  bands at 2960 cm<sup>-1</sup> and 2873 cm<sup>-1</sup>, respectively (cf. Supplementary Fig. 16). The intensities of these CH<sub>3</sub> signals increased with the reaction time on stream (see inset in Fig. 5 and Supplementary Fig. 23). Simultaneously, bands assigned to CH<sub>2</sub> stretching vibrations of LDPE (2913 cm<sup>-1</sup> and 2845 cm<sup>-1</sup>) gradually decreased and shifted to 2902 cm<sup>-1</sup> and 2838 cm<sup>-1</sup> (due to the impact of polymer chain strain on vibrational frequencies), respectively<sup>48</sup>. These observations reflect the deconstruction of LDPE into short alkanes via cracking-alkylation with iC5. Evidently, the prominent increase of methylene rocking and skeletal stretching of  $-(CH_2)_n$  in the regions of 760–900 cm<sup>-1</sup> and 650–680 cm<sup>-1</sup> agrees with the model for the depolymerization process<sup>48,49</sup>. The bands of [C<sub>4</sub>Py] cation and dichloromethane are well preserved, indicating that they are largely not involved in the reaction.

It should be noted that the signals of alkene intermediates are not observed during LDPE cracking (compared to the standard alkene in Supplementary Fig. 24), which matched well with in situ <sup>1</sup>H NMR spectroscopy. To interrogate the presence of alkenes, an iC<sub>5</sub> on-off experiment was performed during the operando IR study (Supplementary Fig. 25). After passing N<sub>2</sub> at 40 min to purge iC<sub>5</sub>, the characteristic bands of conjugated dienes at 1630, 1500, 1482, and 1165 cm<sup>-1</sup> were observed<sup>50</sup>. This indicates that the removal of iC<sub>5</sub> leads to a different reaction pathway, forming acid-soluble conjugated oil (ASO) via oligomerization and hydrogen transfer reactions. We concluded, therefore, that the endothermic and exothermic steps of cracking and alkylation occurred closely coupled, i.e., alkenes formed via cracking rapidly are added to the carbenium ion in the alkylation cycle.

Building on these findings, we proposed a set of key elementary steps (Fig. 6 and Supplementary Fig. 26) initiated by the dissociation of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> to active catalytic AlCl<sub>3</sub> species (Rxn 1). Then, TBC as an initiator, reacted with AlCl<sub>3</sub> to generate initial carbenium ions (Rxn 2). All formed carbenium ion-intermediates should be surrounded and stabilized by the counterpart AlCl<sub>4</sub><sup>-</sup> anions. Then, AlCl<sub>4</sub><sup>-</sup>-coordinated carbenium ions as reactive ion-pair intermediates activate the C-H bonds of hydrocarbons (either LDPE or iC<sub>5</sub>, Rxn 3 and 4), followed by C-H bond cleavage via hydride transfer to preferentially form carbenium ions in the polymer and iC<sub>5</sub>. Next, the formed polyolefinic carbenium ion pairs undergo isomerization and cracking via  $\beta$ -scission, which yields short carbenium ions and alkenes (Rxn 5). Simultaneously, the formed alkenes react with  $iC_5^+$  via the alkylation step, shifting the equilibrium and catalyzing polyolefin conversion (Rxn 6). The long-chain fragments undergo further cracking, and alkylation cycles to the branched alkylate. The PE carbenium ion can be

$Al_2Cl_7 \xrightarrow{\bigcirc} AICl_4 + AICl_3$	(Rxn 1:dissociation)
$AICI_3 + TBC \longleftrightarrow AICI_3 \overset{\frown}{\longrightarrow} CI \overset{\frown}{\longrightarrow} C_4 \overset{\frown}{\longrightarrow} CICI_4 \overset{\bigcirc}{\longleftarrow} AICI_4 \overset{\bigcirc}{\longrightarrow}$	(Rxn 2: CI abstraction)
$C_n + C_4^{\bigoplus} AlCl_4^{\bigoplus} \iff C_n^{\bigoplus} AlCl_4^{\bigoplus} + C_4$	(Rxn 3: H transfer)
$iC_5 + C_4^{\bigoplus} - AICI_4^{\bigoplus} \longrightarrow iC_5^{\bigoplus} - AICI_4^{\bigoplus} + C_4$	(Rxn 4: H transfer)
$C_{n}^{\bigoplus} \cdots AICI_{4}^{\bigoplus} \longrightarrow C_{x}^{=} + C_{n-x}^{\bigoplus} \cdots AICI_{4}^{\bigoplus}$	(Rxn 5: $\beta$ -scission)
$C_x^{=} + iC_5^{\ominus} \cdots AICI_4^{\ominus} \longrightarrow C_{x+5}^{\ominus} \cdots AICI_4^{\ominus}$	(Rxn 6: alkylation)
$C_{x+5}^{\bigoplus} AlCl_4^{\bigoplus} + iC_5 \longrightarrow C_{x+5} + iC_5^{\bigoplus} AlCl_4^{\bigoplus}$	(Rxn 7: H transfer)

Fig. 6 | Proposed sequence of key reaction steps in the cracking-alkylation of polyolefin with iC5 over [C4Py]Cl-2AlCl3. All resulting carbenium ion-intermediates are not bare species but surrounded and stabilized by the counterpart AlCl<sub>4</sub><sup>-</sup> to form ion pairs.

terminated by recombining hydride (Rxn 7). The termination reactions are the reverse of the initiation reactions.

#### Discussion

Thus, the concentration of carbenium ions governs the overall reaction rate, with these intermediates surrounded and stabilized by  $AlCl_4^-$  anions, existing as  $AlCl_3$  adducts via reversible transformation. The total concentrations of  $AlCl_3$  adducts ( $\Sigma[AlCl_3\text{-}adduct]$ ) are equivalent to  $\Delta[AlCl_4^-]$ . Initially, the concentration of carbenium ions corresponds to the TBC loading, which explains the direct correlation between the initial reaction rate, the concentration of TBC loading, and the dissociation of  $Al_2Cl_7^-$  (Supplementary Fig. 11).

Given that cracking and alkylation occurred concurrently and continuously, the initial rate (r) normalized to the total Al adducts concentration can be expressed as Eq. 3 (see detailed derivations in Supplementary Note 3):

$$r_{Al} = \frac{r}{\sum [AlCl_3 - adduct]} = \frac{k_{alkyl}k_{crack}K_{H1}K_{H2}K_{a1}K_{a2}[C_nH_{2n+2}][iC_5H_{12}]}{k_{oligom}K_{H1}K_{a1}[C_nH_{2n+2}] + k_{alkyl}K_{H2}K_{a2}[iC_5H_{12}]}$$
(3)

in which  $[C_nH_{2n+2}]$  and  $[iC_5H_{12}]$  are the concentrations of polyolefin and  $iC_5$ , respectively;  $K_{a1}$  and  $K_{a2}$  denote the equilibrium constants of the association of carbenium ion-pair intermediates with polyolefin and  $iC_5$ , respectively;  $K_{H1}$  and  $K_{H2}$  denote the equilibrium constants of subsequent hydride transfer steps;  $k_{crack}$  and  $k_{oligom}$  are the forward and reverse rate constants of the polyolefin cracking step;  $k_{alkyl}$  denote the rate constant of the alkylation step. We hypothesize that the effects of the environment of carbenium ion-pairs are identical for reacting molecules, i.e., the association equilibrium constants ( $K_a$ ) and the hydride transfer equilibrium constants ( $K_H$ ) of LDPE and  $iC_5$ are identical:  $K_{a1} \approx K_{a2}$  and  $K_{H1} \approx K_{H2}$ , then we have:

$$\frac{1}{r_{Al}} = \frac{1}{k_{crack}K_aK_H[C_nH_{2n+2}]} + \frac{k_{oligom}}{k_{alkyl}k_{crack}K_aK_H[iC_5H_{12}]}$$
(4)

Clearly, the rate of tandem cracking-alkylation depends closely on the combination of the carbenium ion-pairs association equilibrium constants ( $K_a$ ), the hydride transfer equilibrium constants between Al active species and reactants ( $K_H$ ), the cracking and alkylation rate constant ( $k_{crack}$  and  $k_{alkyl}$ ), and the concentrations of reactants. We also plotted  $1/r_{Al}$  against  $1/[C_nH_{2n+2}]$  and  $1/[iC_5H_{12}]$  as well as  $1/[C_{16}]$ , respectively (Supplementary Fig. 27). All experiment data agreed well with Eq. 4. The reciprocal of the  $1/r_{Al}$  increases linearly with the reciprocal of the concentrations of  $[C_nH_{2n+2}]$  and  $[iC_5H_{12}]$ , respectively. In summary, two active species evolve in chloroaluminate ionic liquids during low-temperature kinetically coupled cracking and alkylation of polyolefins with iso-paraffins. Initially, the main species of chloroaluminate ions during operation are the monomer being generated in situ through the dissociation of  $Al_2Cl_7^-$  and its reactive adduct with TBC. The adduct undergoes a reversible transformation into a *tert*-butyl carbenium ion and  $AlCl_4^-$  ion pair. Subsequently, hydride transfer from the formed *tert*-butyl carbenium ion leads to carbenium ions in the alkane polymer strands and eventually in  $IC_5$  (the alkylating agent). Hydride transfer is rapid and facilitated by an environment of high ionic strength. Specifically, the propagation of carbenium ion intermediates by hydride transfer always involves species that are associated and stabilized by  $AlCl_4^-$  anions. Computational study strongly supports these conclusions.

In situ <sup>1</sup>H NMR spectra showed the presence and fluctuation of olefinic intermediates throughout the reaction, which consistently remained at a low concentration of -0.2–0.5%. The introduction of additional olefin as a substitute for TBC exhibited a pronounced preference for oligomerization over alkylation, resulting in no discernible enhancement for LDPE conversion. These findings are in accordance with the operando IR study and kinetic analysis showing that cracking and alkylation occur concertedly. Carbenium ions stabilized within the alkane polymer strands isomerize and later cleave by  $\beta$ -scission, yielding shorter carbenium ions and alkenes. The alkenes formed participate in the alkylation cycle at very high rates by adding to carbenium ions generated from iC<sub>5</sub>.

Taken together, this insight enables the advancement of catalytic transformation of polyolefins and will contribute to the design of a next-generation family of catalysts, facilitating the deconstruction of discarded polyolefins with low energy consumption and a reduced carbon footprint.

#### Methods Chemicals

# All chemicals were purchased from Sigma-Aldrich and directly used without any purification: low-density polyethylene (LDPE, average $M_w \sim 4000$ , average $M_n \sim 1700$ ; Product-No.:427772), n-hexadecane (n-C<sub>16</sub>H<sub>34</sub>, anhydrous, $\geq 99\%$ ), isopentane (anhydrous, $\geq 99\%$ ), N-butylpyridinium chloride ( $\geq 98\%$ ), anhydrous aluminum(III) chloride (99.99 %), trans-decahydronaphthalene (trans-Decalin, 99%), dichloromethane (DCM, $\geq 99.5\%$ ), *tert*-butylchloride (TBC, 99%).

#### Catalyst characterization

X-ray absorption spectroscopy (XAS) measurements at Al K-edge (1560 eV) were measured on the PHOENIX beamline at the Swiss Light Source (SLS) of the Paul Scherrer Institute (Villigen, Switzerland), All spectra were measured in fluorescence mode using a one-element energy dispersive silicon drift diode (KeteK) detector. The measurements were performed using a PTFE liquid flow cell at room temperature. The design of the cell was adapted from the liquid titration cell available at the PHOENIX I end-station. The cell was equipped with a liquid inlet and outlet and a 500 nm thick silicon nitride window. Various [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> ionic liquids with [C<sub>4</sub>Py]Cl:AlCl<sub>3</sub> ratio between 1:1 and 1:2 were prepared inside a glove box. The ionic liquid with [C<sub>4</sub>Py]Cl:AlCl<sub>3</sub> = 1:1 was diluted in DCM as it was a solid at room temperature. Before measurements, the ionic liquids were carefully removed from the glove box with a glass syringe. A syringe pump was then used to fill the liquid flow cell with the ionic liquid. The cell was flushed with DCM followed by nitrogen between two measurements. Beam damage to the samples was assessed by comparing successive measurements and several spectra were averaged to reduce the signalto-noise ratio, X-ray absorption near edge structure (XANES) and extended x-ray absorption fine structure (EXAFS) analyses were performed using Athena and Artemis software packages<sup>51</sup>. All spectra were corrected for self-absorption using the "fluo" algorithm as implemented in Athena. For XANES analyses, the spectra were normalized and flattened. For EXAFS analyses, the spectra were normalized, background subtracted, k<sup>2</sup>-weighted, and Fourier-transformed (FT) in the k-range between  $k = 2.5 \text{ Å}^{-1}$  and  $k = 8.5 \text{ Å}^{-1}$ . EXAFS fitting was performed in k-space, simultaneously on the  $k^{1}$ -,  $k^{2}$ -, and  $k^{3}$ -weighted data in the k-range between  $k = 2.7 \text{ Å}^{-1}$  and  $k = 8.0 \text{ Å}^{-1}$ . The spectra for EXAFS analyses were limited to an upper bound of ~1833 eV (k ~ 8.6 Å<sup>-1</sup>) due the occurrence of Si K-edge at ~1839 eV.

In situ Raman spectra were measured using a Renishaw inVia Reflex Raman System equipped with a 785 nm RL532C laser. The spectrometer was combined with a Leica DM2700M optical light microscope from Leica Microsystems for focusing the Raman laser. The measurement conditions were identical to those in our tube reactor system. The measurement conditions were identical to our tube reactor system. LDPE (200 mg), iC<sub>5</sub>(800 mg), TBC (5 mg) and 2 mmol ionic liquids (2 mmol) diluted in 3 ml DCM were added into the borosilicate glass. The reactor was then heated to 60 °C with magnetic stirring at 1200 rpm. Note that there is quick phase separation without stirring, in which the ionic liquid and DCM phase are on the bottom. Therefore, the laser beam was directly focused on the bottom of the glass reactor by a × 5 objective with a maximum laser power of 1.0 mW to avoid laser-induced sample degradation during the measurement. The spectra were collected every 5 min (Exposure time: 1s, Laser Power: 50 %, accumulations: 20 times) for a total duration of 180 min.

In situ <sup>27</sup>Al magic-angle spinning nuclear magnetic resonance (<sup>27</sup>Al MAS NMR) spectroscopy measurements were conducted on a Varian-Agilent Inova wide-bore 300 MHz NMR spectrometer with a commercial 7.5 mm Vespel pencil-type MAS probe. The spectrometer operated at <sup>27</sup>Al Larmor frequencies of 78.204 MHz. Sample spinning at -4 kHz enabled the acquisition of high-resolution MAS NMR spectra. A specialized in situ MAS NMR rotor was utilized to ensure the proper sealing of a mixture at elevated temperature and pressure<sup>52</sup>. The sample cell space volume was -300 µL. For acquiring the <sup>27</sup>Al signal, a single-pulse sequence was utilized, comprising a 5 µs pulse width (equivalent to a pulse angle of 50°), an acquisition time of 50 ms, and a recycle delay of 0.5 s. All spectra were referenced externally to a 1 M Al(NO<sub>3</sub>)<sub>3</sub> (0 ppm) aqueous solution<sup>53</sup>.

The <sup>27</sup>Al spectra are deconvoluted into two resonances centered at 103 and 97 ppm through standard background subtraction and fitting the experimental curve to a combination of Lorentzian and Gaussian lines. The integrated line widths were calculated by summing up the full width at half maximum (FWHM) of individual peaks.

Ex situ <sup>27</sup>AI MAS NMR experiments were conducted using a Varian-Agilent Inova 63 mm wide-bore 850 MHz NMR spectrometer. A commercial 3.2 mm pencil-type MAS probe was employed, enabling the use of ~15 mg of sample for each experiment. For acquiring each <sup>27</sup>Al MAS NMR spectrum, a single-pulse sequence was utilized with a pulse length of 0.4 us, corresponding to a pulse angle of 45°. The experiments had a recycle time of 1 s and a total accumulation of 5000 scans. All spectra were acquired at a sample spinning rate of 20 kHz  $\pm$  2 Hz and were referenced to 1.5 M Al(NO<sub>3</sub>)<sub>3</sub> in H<sub>2</sub>O (0 ppm), using the center of the octahedral peak of solid  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (at 13.8 ppm) as a secondary reference. To ensure the accuracy of the measurements, the weights of the samples loaded into the MAS rotor were recorded, and four spectra were acquired to verify the stability of the spectrometer. The matching and tuning conditions of the radiofrequency (RF) circuit of the NMR probe were established using a network analyzer. All other experimental conditions were kept identical for all analyzed samples. By normalizing the absolute peak areas to the sample mass and plotting them against the known Al concentration from elemental analysis, a calibration factor was obtained. The spectra were analyzed using the NUTS NMR data processing software (Acorn NMR Inc.).

In situ <sup>1</sup>H NMR experiments were conducted using a Bruker NEO console and stack, coupled with a 500 MHz Oxford magnet and equipped with a Bruker PI HR-BBO500S2-BBF/H/D-5.0-Z SP probe. The conversion of n-hexadecane (n-C<sub>16</sub>) was monitored using <sup>1</sup>H NMR spectroscopy in mixtures of  $[C_4Py]$ -2AlCl<sub>3</sub>, iC<sub>5</sub>, TBC, and CD<sub>2</sub>Cl<sub>2</sub>. In a typical experiment, an NMR tube was loaded with  $[C_4Py]$ -2AlCl<sub>3</sub> (100 mg, 0.23 mmol), C<sub>16</sub> (35 mg, 0.16 mmol or 2.5 mmol C), and TBC (0.5 µmol, corresponding to 0.2 mol% relative to  $[C_4Py]$ -2AlCl<sub>3</sub>). Varying amounts of isopentane (iC<sub>5</sub>) ranging from 0 to 0.9 mmol were incrementally added under the established reaction conditions while maintaining all other quantities constant. The data were recorded with a 400 MHz spectrometer.

The operando IR spectra were recorded using a ReactIR<sup>™</sup> 45 m spectrometer (Mettler Toledo) connected to a 150 mL Parr autoclave at 60 °C. The bottom of the autoclave contains a probing window that is connected to the sentinel probe through the conduit K4, which allows the collection of the operando IR spectra in the liquid phase at different temperatures. Before these tests, a background spectrum was collected at 60 °C under a vacuum. Then, the autoclave reactor was loaded with the LDPE (2.0 g), iC<sub>5</sub> (8.0 g), ionic liquids (20 mmol) diluted in30 ml DCM, and TBC (50 mg) as an additive, followed by flushing with nitrogen to remove atmospheric carbon dioxide. The reactor was heated, and the stirring started once the temperature reached 60 °C with a mechanical stirring speed of 700 rpm. The spectra with 4 cm<sup>-1</sup> resolution were collected every 15 s for a total duration of 240 min, and each spectrum was scanned 256 times.

## Preparation of N-butyl pyridinium chloride-aluminum chloride ionic liquid ([C4Py]Cl-xAlCl3) preparation

A series of  $[C_4Py]Cl$ -xAlCl<sub>3</sub> ionic liquids prepared by mixing N-butyl pyridinium chloride( $[C_4Py]Cl$ ) and anhydrous aluminum chloride at different molar ratios (1.0, 1.2, 1.4, 1.6, 1.8, 2.0 and 2.5) in a glove box. In a typical synthesis of  $[C_4Py]Cl$ -2AlCl<sub>3</sub> ionic liquid, anhydrous aluminum chloride (6 mmol) was slowly added to  $[C_4Py]Cl$  (3 mmol) in a DURAN<sup>®</sup> borosilicate glass tube at room temperature, yielding a light-gray liquid<sup>21</sup>.

## Catalytic tandem cracking-alkylation reaction of polyolefin with isopentane

The tandem cracking-alkylation reaction of polyolefin with isopentane was carried out in a 30 mL DURAN<sup>®</sup> borosilicate glass tube (equipped with an open-top screw cap with silicone liner). In a typical reaction, LDPE (200–800 mg) iC<sub>5</sub> (200–800 mg), and TBC (5 mg, as an additive) are added into the glass tube containing [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> ionic liquids diluted in dichloromethane. Then, the reactor was heated up to

specified temperatures under magnetic stirring (1200 rpm). For the kinetic studies, identical reactions were run in parallel at different time intervals. After the reaction, the glass tube was cooled to -25 °C, resulting in a biphasic system. Notably, a scaled-up reaction to 150 ml Parr autoclave produced identical results, allowing operando IR measurements (See Supplementary Fig. 21).

The headspace of the reactor was first analyzed using a gas chromatograph equipped with Supel-Q<sup>™</sup> PLOT fused silica capillary column (30 m  $\times$  0.53 mm  $\times$  2.0  $\mu$ m) and a mass spectrometer. Then, an additional 2 ml of isopentane as an extracting agent was injected into the tube (cooled to -25 °C), enabling a complete phase separation. The ionic liquid phase under the bottom was then transferred to a glass vial and quenched by NaOH aqueous solution at low temperature, in which organic residues were extracted by chloroform and analyzed by GCmass spectrometry. The organic phase was then mixed with 15 mg of trans-decalin as an external standard and 1 ml chloroform for promoting the mixing of organic products, followed by GC and GC-MS analyses. The unreacted solids were separated by filtration to quantify the solid conversion. The sum of all detected products was taken as the total vield. The response factor for alkanes of each carbon number and the corresponding retention time were calibrated using n-alkane standard (C7- C40, Supeco-49452-U). The unreacted LDPE suspended solids were separated from the top phase by a simple filtration to quantify the conversion.

Converson, selectivity, yield and the initial rate (r) were calculated according to the following equations:

$$Conversion = \left(1 - \frac{mass \ of \ residual \ LDPE}{initial \ mass \ of \ LDPE}\right) \times 100\%$$
(5)

$$Yield(Ci,\%) = \left(\frac{\sum Area(C_i)}{Area(external \ standard)} \times \frac{mass \ of \ external \ standard}{initial \ mass \ of \ LDPE}\right) \times 100\%$$
(6)

$$r = \frac{\text{initial mass of LDPE} - \text{mass of residual LDPE}}{\text{reaction time}(t)}$$
(7)

where  $\sum Area(C_i)$  is the sum of GC areas of  $C_i$ , in which all peaks between n- $C_{i-1}$  and n- $C_i$  were assumed as branched  $C_i$  alkanes unless GC-MS suggested otherwise. Area (external standard) is the GC area of the external standard. Note that all products and external standard are saturated hydrocarbons; the relative response factors for each species were assumed to be 1.0. We studied the rates at low conversions <20 wt.%, and the carbon balances were >95 %.

The concentration of AlCl<sub>3</sub> in  $[C_4Py]Cl-xAlCl_3$  ( $x \in [1,2]$ ) at spectific reaction time (t) was calculated using Eqs. 1–2 in the main text (see detailed derivations in Supplementary Note 2).

#### Density functional theory calculations for XAS and Raman

All density functional theory (DFT) calculations were carried out using ORCA quantum chemistry package version 5.3<sup>54</sup>. Geometry optimizations and vibrational frequency calculations utilized Ahlrichs def2-TZVP basis sets and auxiliary basis sets SARC/J<sup>55,56</sup>. The B3LYP hybrid-GGA functional was employed for all calculations, along with the atom pairwise dispersion correction and the Becke-Johnson damping scheme (D3BJ)<sup>57</sup>. To enhance computational efficiency, the RIJCOSX approximation was also applied<sup>58</sup>. X-ray absorption spectra of the optimized structures were simulated using time-dependent density functional theory (TDDFT) with the Tamm-Dancoff approximation, allowing for transitions from Al 1 s orbitals. Up to 150 roots were calculated, allowing for transitions generic dipole and electric quadrupole contributions. All calculations were performed with a conductor-like polarizable continuum model (CPCM) using DCM as solvent<sup>58</sup>.

#### Density functional theory calculations for<sup>27</sup>Al MAS NMR

Quantum chemistry calculations of <sup>27</sup>Al chemical shifts were utilized to aid in the interpretation of NMR spectra using the Amsterdam Density Functional (ADF) software<sup>59,60</sup>. The cluster models were optimized using the Beck-Lee-Yang-Parr functional<sup>61</sup>, and a Slater-type, all electron, triple-  $\zeta$ , two-polarization function (TZ2P) was utilized<sup>62</sup>. To correlate the calculated nuclear shielding from DFT to the observed NMR chemical shifts, [C<sub>4</sub>Py]Cl-IAlCl<sub>3</sub> was used as the computational standard at 103 ppm, serving as a secondary reference to 1.0 M Al(NO<sub>3</sub>)<sub>3</sub> (0 ppm) due to its unique narrow peak identified in experiments. The calculated nuclear shielding of other models was converted to an experimental chemical shift scale using the formula  $\delta_{obs} = 443.84$ - $\delta_{calc} + 103.0$  ppm.

#### AIMD simulations and reaction free energy calculations

To achieve a well-equilibrated structure at 70 °C, a model system was constructed, comprising 1 n-C<sub>16</sub>H<sub>34</sub>, 2 [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub> ionic liquids ([C<sub>4</sub>Py]<sup>+</sup>-Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>), 6 iC<sub>5</sub>, 1 TBC, and 105 DCM in a 23 Å cubic cell, mimicking experimental compositions. Subsequently, DFT-based ab initio molecular dynamics (AIMD) simulations were conducted with periodic boundary conditions (3D PBC) using the generalized gradient approximation (GGA) with Perdew, Burke, and Ernzerhoff (PBE) exchange-correlation functionals<sup>63</sup>, and Grimme's third-generation (DFT-D3) dispersion correction<sup>64</sup>, as implemented in the CP2K package<sup>65</sup>. The core were described electrons using Goedecker-Teter-Hutter (GTH) pseudopotentials<sup>66</sup>, while the valence wavefunctions were expanded in optimized double-ζ Gaussian basis sets. An auxiliary plane wave basis set with a cutoff energy of 400 Ry was employed for the calculation of the electrostatic terms. Due to the substantial size of the supercell, the  $\Gamma$ -point approximation was used for the Brillouin zone integration.

AIMD simulations were performed by sampling the NVT canonical ensemble with a Nosé–Hoover thermostat chain, using a time step of 0.5 fs at 70 °C. After ~60 ps of simulation, an equilibrated structure was obtained from the last frame. Subsequently, AIMD-based Blue Moon ensemble calculations<sup>67</sup> were performed by constraining the distance between two specified atoms from the reacting molecules. The integration of the ensemble-averaged force due to the constraints along the reaction coordinate generated a free energy profile as a function of distance, providing the standard Helmholtz free energy ( $\Delta$ F°) and activation energy ( $E_a$ ).

#### Data availability

All data are available within the article and its Supplementary Information files and from the authors upon request. Source data are provided in this paper.

#### References

- Vollmer, I. et al. Beyond mechanical recycling: giving new life to plastic waste. Angew. Chem. Int. Ed. 59, 15402–15423 (2020).
- Kosloski-Oh, S. C., Wood, Z. A., Manjarrez, Y., de los Rios, J. P. & Fieser, M. E. Catalytic methods for chemical recycling or upcycling of commercial polymers. *Mater. Horiz.* 8, 1084–1129 (2021).
- Martín, A. J., Mondelli, C., Jaydev, S. D. & Pérez-Ramírez, J. Catalytic processing of plastic waste on the rise. *Chem* 7, 1487–1533 (2021).
- U.S. Energy Information Administration (EIA). Refinery Capacity Report, Form EIA-820 https://www.eia.gov/petroleum/ refinerycapacity/ (2022).
- Yeung, C. W. S., Teo, J. Y. Q., Loh, X. J. & Lim, J. Y. C. Polyolefins and polystyrene as chemical resources for a sustainable future: challenges, advances, and prospects. ACS Mater. Lett.3, 1660–1676 (2021).
- Chu, M., Liu, Y., Lou, X., Zhang, Q. & Chen, J. Rational design of chemical catalysis for plastic recycling. ACS Catal. 12, 4659–4679 (2022).

#### Article

- Kaminsky, W. & Zorriqueta, I.-J. N. Catalytical and thermal pyrolysis of polyolefins. J. Anal. Appl. Pyrolysis 79, 368–374 (2007).
- 8. Zichittella, G. et al. Hydrogenolysis of polyethylene and polypropylene into propane over cobalt-based catalysts. *JACS Au* **2**, 2259–2268 (2022).
- 9. Rorrer, J. E. et al. Role of bifunctional Ru/acid catalysts in the selective hydrocracking of polyethylene and polypropylene waste to liquid hydrocarbons. *ACS Catal.* **12**, 13969–13979 (2022).
- Liu, S., Kots, P. A., Vance, B. C., Danielson, A. & Vlachos, D. G. Plastic waste to fuels by hydrocracking at mild conditions. *Sci. Adv.* 7, eabf8283 (2021).
- 11. Wang, C. et al. Polyethylene hydrogenolysis at mild conditions over ruthenium on tungstated zirconia. *JACS Au* **1**, 1422–1434 (2021).
- 12. Duan, J. et al. Coking-resistant polyethylene upcycling modulated by zeolite micropore diffusion. *J. Am. Chem.* Soc. **144**, 14269–14277 (2022).
- 13. Chen, S. et al. Ultrasmall amorphous zirconia nanoparticles catalyse polyolefin hydrogenolysis. *Nat. Catal.* **6**, 161–173 (2023).
- Zhang, F. et al. Polyethylene upcycling to long-chain alkylaromatics by tandem hydrogenolysis/aromatization. *Science* **370**, 437–441 (2020).
- 15. Conk, R. J. et al. Catalytic deconstruction of waste polyethylene with ethylene to form propylene. *Science* **377**, 1561–1566 (2022).
- Jia, X., Qin, C., Friedberger, T., Guan, Z. & Huang, Z. Efficient and selective degradation of polyethylenes into liquid fuels and waxes under mild conditions. Sci. Adv. 2, e1501591 (2016).
- Wang, N. M. et al. Chemical recycling of polyethylene by tandem catalytic conversion to propylene. *J. Am. Chem. Soc.* **144**, 18526–18531 (2022).
- Gao, J., Zhu, L. & Conley, M. P. Cationic tantalum hydrides catalyze hydrogenolysis and alkane metathesis reactions of paraffins and polyethylene. *J. Am. Chem.* Soc. **145**, 4964–4968 (2023).
- Ellis, L. D. et al. Chemical and biological catalysis for plastics recycling and upcycling. *Nat. Catal.* 4, 539–556 (2021).
- Tennakoon, A. et al. Catalytic upcycling of high-density polyethylene via a processive mechanism. *Nat. Catal.* 3, 893–901 (2020).
- Zhang, W. et al. Low-temperature upcycling of polyolefins into liquid alkanes via tandem cracking-alkylation. Science **379**, 807–811 (2023).
- Kore, R., Scurto, A. M. & Shiflett, M. B. Review of isobutane alkylation technology using ionic liquid-based catalysts—where do we stand? *Ind. Eng. Chem. Res.* 59, 15811–15838 (2020).
- Plechkova, N. V. & Seddon, K. R. Applications of ionic liquids in the chemical industry. *Chem. Soc. Rev.* 37, 123–150 (2008).
- 24. Estager, J., Holbrey, J. D. & Swadźba-Kwaśny, M. Halometallate ionic liquids—revisited. *Chem. Soc. Rev.* **43**, 847–886 (2014).
- Brown, L. C., Hogg, J. M. & Swadźba-Kwaśny, M. Lewis Acidic Ionic Liquids. Top. Curr. Chem. (Z.) 375, 78 (2017).
- Timken, H. K., Luo, H., Chang, B.-K., Carter, E. & Cole, M. ISOALKY™ technology: next-generation alkylate gasoline manufacturing process technology using ionic liquid catalyst. In *Commercial applications of ionic liquids. green chemistry and sustainable technology.* (ed. Shiflett, M.) 33–47 https://doi.org/10.1007/978-3-030-35245-5\_2 (Springer, Cham, 2020).
- Feller, A. & Lercher, J. A. Chemistry and technology of isobutane/ alkene alkylation catalyzed by liquid and solid acids. *Adv. Catal.* 48, 229–295 (2004).
- Aschauer, S., Schilder, L., Korth, W., Fritschi, S. & Jess, A. Liquidphase isobutane/butene-alkylation using promoted lewis-acidic ilcatalysts. *Catal. Lett.* **141**, 1405–1419 (2011).
- Kore, R., Mishra, M. K., Gonela, U. M. & Rogers, R. D. Chloroaluminate liquid clathrates: is it the cations or the anions that drive the solubility of aromatics? *Ind. Eng. Chem. Res.* 59, 18419–18424 (2020).

- Pan, C. et al. Energy storage mechanisms in high-capacity graphitic c3n4 cathodes for al-ion batteries. J. Phys. Chem. C. 124, 10288–10297 (2020).
- Zhang, J., Huang, C., Chen, B., Ren, P. & Pu, M. Isobutane/2-butene alkylation catalyzed by chloroaluminate ionic liquids in the presence of aromatic additives. J. Catal. 249, 261–268 (2007).
- 32. Wen, X. et al. Materials compatibility in rechargeable aluminum batteries: chemical and electrochemical properties between vanadium pentoxide and chloroaluminate ionic liquids. *Chem. Mater.* **31**, 7238–7247 (2019).
- Angell, M. et al. High Coulombic efficiency aluminum-ion battery using an AlCl<sub>3</sub>-urea ionic liquid analog electrolyte. *Proc. Nat. Acad. Sci.* **114**, 834–839 (2017).
- Kim, I., Jang, S., Lee, K. H., Tak, Y. & Lee, G. In situ polymerized solid electrolytes for superior safety and stability of flexible solid-state Alion batteries. *Energy Storage Mater.* 40, 229–238 (2021).
- Ferrara, C., Dall'Asta, V., Berbenni, V., Quartarone, E. & Mustarelli, P. Physicochemical characterization of alcl3–1-ethyl-3-methylimidazolium chloride ionic liquid electrolytes for aluminum rechargeable batteries. J. Phys. Chem. C. **121**, 26607–26614 (2017).
- Wu, G., Liu, Y., Liu, G., Hu, R. & Gao, G. Role of aromatics in isobutane alkylation of chloroaluminate ionic liquids: Insights from aromatic – ion interaction. J. Catal. 396, 54–64 (2021).
- Dembowski, M. et al. Influence of soluble oligomeric aluminum on precipitation in the Al-KOH-H2O system. *Phys. Chem. Chem. Phys.* 22, 24677–24685 (2020).
- Gray, J. L. & Maciel, G. E. Aluminum-27 nuclear magnetic resonance study of the room-temperature melt aluminum trichloride butylpyridinium chloride. J. Am. Chem. Soc. **103**, 7147–7151 (1981).
- Coleman, F., Srinivasan, G. & Swadźba-Kwaśny, M. Liquid coordination complexes formed by the heterolytic cleavage of metal halides. *Angew. Chem. Int. Ed.* 52, 12582–12586 (2013).
- 40. Shen, X. et al. Ultra-fast charging in aluminum-ion batteries: electric double layers on active anode. *Nat. Commun.* **12**, 820 (2021).
- Angell, M., Zhu, G., Lin, M.-C., Rong, Y. & Dai, H. Ionic liquid analogs of alcl3 with urea derivatives as electrolytes for aluminum batteries. *Adv. Funct. Mater.* **30**, 1901928 (2020).
- 42. Jach, F. et al. A low-cost al-graphite battery with urea and acetamide-based electrolytes. *ChemElectroChem* **8**, 1988–1992 (2021).
- Ng, K. L., Dong, T., Anawati, J. & Azimi, G. High-performance aluminum ion battery using cost-effective alcl3-trimethylamine hydrochloride ionic liquid electrolyte. *Adv. Sustain. Syst.* 4, 2000074 (2020).
- Zhang, W. et al. Chloride and hydride transfer as keys to catalytic upcycling of polyethylene into liquid alkanes. *Angew. Chem. Int. Ed.* 63, e202319580 (2024).
- Wu, L. et al. Aluminum species and the synthesis mechanism of AlCl<sub>3</sub>-CuCl-arene solutions. *Ind. Eng. Chem. Res.* 60, 1155–1163 (2021).
- Pfriem, N. et al. Role of the ionic environment in enhancing the activity of reacting molecules in zeolite pores. *Science* **372**, 952 (2021).
- 47. Smith, B. The infrared spectra of polymers ii: polyethylene. Spectroscopy **36**, 24–29 (2021).
- 48. Noda, I., Dowrey, A., Haynes, J. & Marcott, C. in *Physical Properties Of Polymers Handbook* 395–406 (Springer, 2007).
- 49. Li, H.-W., Strauss, H. L. & Snyder, R. G. Differences in the IR methylene rocking bands between the crystalline fatty acids and n-alkanes: frequencies, intensities, and correlation splitting. *J. Phys. Chem. A* **108**, 6629–6642(2004).
- 50. Li, Y. et al. Characterization and hydrogenation removal of acidsoluble oil in ionic liquid catalysts for isobutane alkylation. *Ind. Eng. Chem. Res.* **60**, 13764–13773 (2021).

#### Article

- 51. Ravel, B. & Newville, M. ATHENA, ARTEMIS, HEPHAESTUS: data analysis for X-ray absorption spectroscopy using IFEFFIT. *J. Synchrotron Radiat.* **12**, 537–541 (2005).
- Jaegers, N. R., Mueller, K. T., Wang, Y. & Hu, J. Z. Variable temperature and pressure operando MAS NMR for catalysis science and related materials. Acc. Chem. Res. 53, 611–619 (2020).
- 53. Jaegers, N. R., Hu, W., Wang, Y. & Hu, J. Z. High-temperature and high-pressure in situ magic angle spinning nuclear magnetic resonance spectroscopy. *J. Vis. Exp.* **164**, e61794 (2020).
- 54. Neese, F. Software update: The ORCA program system—version 5.0. WIREs Comput. Mol. Sci. 12, e1606 (2022).
- Weigend, F. & Ahlrichs, R. Balanced basis sets of split valence, triple zeta valence and quadruple zeta valence quality for H to Rn: design and assessment of accuracy. *Phys. Chem. Chem. Phys.* 7, 3297–3305 (2005).
- Weigend, F. Accurate Coulomb-fitting basis sets for H to Rn. Phys. Chem. Chem. Phys. 8, 1057–1065 (2006).
- Price, A. J. A., Bryenton, K. R. & Johnson, E. R. Requirements for an accurate dispersion-corrected density functional. *J. Chem. Phys.* 154, 230902 (2021).
- Barone, V. & Cossi, M. Quantum calculation of molecular energies and energy gradients in solution by a conductor solvent model. J. Phys. Chem. A **102**, 1995–2001 (1998).
- 59. te Velde, G. et al. Chemistry with ADF. J. Comput. Chem. 22, 931–967 (2001).
- Hu, W. et al. Modelling complex molecular interactions in catalytic materials for energy storage and conversion in nuclear magnetic resonance. *Front. Catal.* 2, 935174 (2022).
- Lee, C., Yang, W. & Parr, R. G. Development of the Colle-Salvetti correlation-energy formula into a functional of the electron density. *Phys. Rev. B* 37, 785–789 (1988).
- 62. Van Lenthe, E. & Baerends, E. J. Optimized slater-type basis sets for the elements 1–118. *J. Comput. Chem.* **24**, 1142–1156 (2003).
- Perdew, J. P., Burke, K. & Ernzerhof, M. Generalized gradient approximation made simple. *Phys. Rev. Lett.* 77, 3865–3868 (1996).
- Grimme, S., Hujo, W. & Kirchner, B. Performance of dispersioncorrected density functional theory for the interactions in ionic liquids. *Phys. Chem. Chem. Phys.* 14, 4875–4883 (2012).
- Kühne, T. D. et al. CP2K: An electronic structure and molecular dynamics software package—quickstep: efficient and accurate electronic structure calculations. *J. Chem. Phys.* **152**, 194103 (2020).
- Goedecker, S., Teter, M. & Hutter, J. Separable dual-space Gaussian pseudopotentials. *Phys. Rev. B* 54, 1703–1710 (1996).
- Carter, E. A., Ciccotti, G., Hynes, J. T. & Kapral, R. Constrained reaction coordinate dynamics for the simulation of rare events. *Chem. Phys. Lett.* **156**, 472–477 (1989).

#### Acknowledgements

We thank Dr. Camelia N. Borca from the Phoenix beamline at the Swiss Light Source (SLS) of the Paul Scherrer Institute in Switzerland for their assistance in Al XAS characterization. We also thank G. L. Haller (Yale University), J. G. Chen (Columbia University), S. L. Scott (UC Santa Barbara), and M. L. Sarazen (Princeton University) for their discussion of the manuscript and helpful suggestions. J.A.L., W.Z., S.K., L. H., W.H., J.M., B.Y., O.Y.G., D.R., J.F., D.M.C., J.H., H.W., and M.L. thank the U.S. Department of Energy (DOE), Office of Science, Office of Basic Energy Sciences (BES), Division of Chemical Sciences, Geosciences and Biosciences (towards a polyolefin-based refinery: understanding and controlling the critical reaction steps, FWP 78459) for funding support. J.H also thank the U.S. Department of Energy (DOE), Office of Science, Office of Basic Energy Sciences (BES), Division of Chemical Sciences, Geosciences and Biosciences (Multifunctional Catalysis to Synthesize and Utilize Energy Carrier, FWP 47319) for funding support of in situ NMR work. Computational work was performed using the National Energy Research Scientific Computing Center located at the Lawrence Berkley National Laboratory provided by a user proposal and the Research Computing Facility at PNNL.

#### **Author contributions**

W.Z. and J.A.L. conceived the research; W.Z., C.Y., Y.S., and P.Z. performed the experiments and the in-situ Raman and operando IR characterizations. L.H., J.H., S.K., and W.H. provided data on the in-situ NMR measurements; R.K. and L.W. performed the XAS characterization; M.-S.L. and D.R. performed AIMD simulations along with the Blue Moon ensemble method. J.F., H.W., O.Y.G., D.M.C., J.M., and B.Y. cooperated with the discussion and provided valuable suggestions. The manuscript was written through the contributions of all authors. All authors have approved the final version of the manuscript.

#### **Competing interests**

The Authors declare no competing interests.

#### **Additional information**

**Supplementary information** The online version contains supplementary material available at https://doi.org/10.1038/s41467-024-49827-4.

**Correspondence** and requests for materials should be addressed to Wei Zhang or Johannes A. Lercher.

**Peer review information** *Nature Communications* thanks Emma McCrea and the other, anonymous, reviewer for their contribution to the peer review of this work. A peer review file is available.

## **Reprints and permissions information** is available at http://www.nature.com/reprints

**Publisher's note** Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional affiliations.

**Open Access** This article is licensed under a Creative Commons Attribution 4.0 International License, which permits use, sharing, adaptation, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons licence, and indicate if changes were made. The images or other third party material in this article are included in the article's Creative Commons licence, unless indicated otherwise in a credit line to the material. If material is not included in the article's Creative Commons licence and your intended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder. To view a copy of this licence, visit http://creativecommons.org/ licenses/by/4.0/.

© Battelle Memorial Institute and The Authors 2024

# **Supplementary Information**

# Active species in chloroaluminate ionic liquids catalyzing lowtemperature polyolefin deconstruction

Wei Zhang,<sup>1,2</sup>\* Rachit Khare,<sup>2</sup> Sungmin Kim,<sup>1 2</sup> Lillian Hale,<sup>1</sup> Wenda Hu,<sup>1</sup> Chunlin Yuan,<sup>2</sup> Yaoci Sheng,<sup>2</sup> Peiran Zhang,<sup>2</sup> Lennart Wahl,<sup>2</sup> Jiande Mai,<sup>1</sup> Boda Yang,<sup>1</sup> Oliver Y. Gutiérrez,<sup>1</sup> Debmalya Ray,<sup>1</sup> John Fulton,<sup>1</sup> Donald M. Camaioni,<sup>1</sup> Jianzhi Hu,<sup>1,3</sup> Huamin Wang,<sup>1</sup> Mal-Soon Lee<sup>1</sup> and Johannes A. Lercher<sup>1,2</sup>\*

 <sup>1</sup> Institute for Integrated Catalysis, Pacific Northwest National Laboratory, P.O. Box 999, Richland, WA99352, USA
 <sup>2</sup> Department of Chemistry and Catalysis Research Center, Technische Universität München, Lichtenbergstr. 4, 85747, Garching, Germany
 <sup>3</sup> The Gene and Linda Voiland School of Chemical Engineering and Bioengineering, Washington State University, Pullman, WA 99164, USA

\*To whom correspondence should be addressed: Wei Zhang (wzhangx@outlook.com); Johannes A. Lercher (johannes.lercher@ch.tum.de)

### Table of Contents

Supplementary Fig. 1   Relationship between initial LDPE conversion rate, the mole fraction ( $\chi$ ) of Al <sub>2</sub> Cl <sub>7</sub> <sup>-</sup> , and empirical [AlCl <sub>3</sub> ] concentration (K*[AlCl <sub>3</sub> ])
Supplementary Note 1: The X-ray absorption spectroscopy and evaluation of chloroaluminate species in ionic liquids
Supplementary Fig. 2   The X-ray absorption spectroscopy and quantitative evaluation of chloroaluminate species in ionic liquids
Supplementary Table 1. Fitting parameters for the EXAFS of [C <sub>4</sub> Py]Cl-xAlCl <sub>3</sub> ionic liquids with varying AlCl <sub>3</sub> :[C <sub>4</sub> Py]Cl molar ratios
Supplementary Fig. 3   The corresponding Al–Cl coordination numbers and interatomic distances obtained from EXAFS fit
Supplementary Fig. 4   Al K-edge EXAFS of [C4Py]Cl-xAlCl <sub>3</sub> ionic liquids (x=1, 1.3, and 1.4). 8
Supplementary Fig. 5   Al K-edge EXAFS of $[C_4Py]Cl-xAlCl_3$ ionic liquids (x=1.5, 1.6, and 1.7). 9
Supplementary Fig. 6   Al K-edge EXAFS of [C <sub>4</sub> Py]Cl- <i>x</i> AlCl <sub>3</sub> ionic liquids (x=1.8, 1.9, and 2).10
Supplementary Fig. 7   Temperature-programmed <sup>27</sup> Al MAS NMR spectroscopy on chloroaluminate ionic liquids
Supplementary Fig. 8   DFT-NMR modeling of Al <sub>2</sub> Cl <sub>7</sub> <sup>-</sup> showing a broadened linewidth in the <sup>27</sup> Al MAS NMR spectra
Supplementary Fig. 9   Raman spectra of [C <sub>4</sub> Py]Cl-xAlCl <sub>3</sub> (x=1-2)13
Supplementary Note 2: Derivations of concentration of $AlCl_4^-$ and $Al_2Cl_7^-$ ( $Al_2Cl_7^- \rightarrow AlCl_4^- + AlCl_3$ ) over various time intervals (t)
Supplementary Fig. 10   The computational simulation of the dissociation of $Al_2Cl_7^-$ in a DCM solvent. 17
Supplementary Fig. 11   Chloroaluminate transformation in the presence of TBC
Supplementary Fig. 12   Raman spectroscopy analysis of the interaction between TBC and [C <sub>4</sub> Py]Cl-xAlCl <sub>3</sub>
Supplementary Fig. 13   The conversion of LDPE plotted against the corresponding variation of chloroaluminate species in ionic liquids
Supplementary Fig. 14   In situ Raman spectra recorded during the cracking-alkylation of $n$ -C <sub>16</sub> H <sub>34</sub> and iC <sub>5</sub> in the presence of TBC
Supplementary Fig. 15   The computational simulations of $Al_2Cl_7^-$ catalyzed hydride abstraction from $iC_5$ .

Supplementary Fig. 16   Computational simulation of AlCl <sub>3</sub> -TBC adduct catalyzing hydride abstraction from nC <sub>16</sub>
Supplementary Fig. 17   In situ 1H NMR spectra of tandem cracking-alkylation of n-C <sub>16</sub> and iC <sub>5</sub> over [C <sub>4</sub> Py]Cl- 2AlCl <sub>3</sub>
Supplementary Fig. 18   Raman spectroscopy analysis of the interaction between TBC and [C <sub>4</sub> Py]Cl-2AlCl <sub>3</sub> .
Supplementary Fig. 19   Time-resolved conversion profile of LDPE in the presence of TBC or $C_5^=$ as additives, compared to conditions without additives
Supplementary Fig. 20   Computed reaction pathway for the formation of AlCl <sub>3</sub> -C <sub>5</sub> <sup>=</sup> adduct. 27
Supplementary Fig. 21   Operando IR setup combing a ReactIRTM 45m spectrometer28
Supplementary Fig. 22   Operando IR spectra were recorded during LDPE depolymerization in the absence of iC <sub>5</sub> over [C <sub>4</sub> Py]Cl-2AlCl <sub>3</sub>
Supplementary Fig. 23   Three-dimensional operando IR spectra of the <i>sp</i> <sup>3</sup> C–H vibrations as a function of reaction time, recorded during LDPE depolymerization in the presence of iC <sub>5</sub> over [C <sub>4</sub> Py]Cl-2AlCl <sub>3</sub> at 60 °C
Supplementary Fig. 25   Operando IR spectra of the iC5 on-off experiment
Supplementary Note 3: Derivations of rate equations in the cracking-alkylation of polyolefin with $iC_5$ over $[C_4Py]Cl-xAlCl_3$
Supplementary Fig. 26   Proposed sequence of key reaction steps in the cracking-alkylation of polyolefin with iC <sub>5</sub> over [C <sub>4</sub> Py]Cl-xAlCl <sub>3</sub>
Supplementary Fig. 27   Kinetic analysis of cracking-alkylation cycles of polyolefin with iC <sub>5</sub> .36



**Supplementary Fig. 1** | Relationship between initial LDPE conversion rate, the mole fraction ( $\chi$ ) of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>, and empirical [AlCl<sub>3</sub>] concentration (K\*[AlCl<sub>3</sub>]).

# Supplementary Note 1: The X-ray absorption spectroscopy and evaluation of chloroaluminate species in ionic liquids

Chloroaluminate ionic liquids were prepared by mixing anhydrous AlCl<sub>3</sub> with N-butyl pyridinium chloride at various ratios. The samples are denoted as ([C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub>, wherein x represents the molar ratio of AlCl<sub>3</sub> and [C<sub>4</sub>Py]Cl (see the experimental section for details). Al K-edge X-ray absorption near edge structure (XANES, Supplementary Fig. 2a) of [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> ionic liquids showed a systematic increase in the pre-edge feature at ~1559.4 eV and a corresponding decrease in the intensity of the white line at ~1560.9 eV as the AlCl<sub>3</sub>/ $[C_4Py]$ Cl molar ratio increased. The increase in the intensity of the pre-edge feature can be attributed to a systematic change in the symmetry of Cl<sup>-</sup> ions coordinating Al. The DFT geometry optimization (Supplementary Fig. 2b) suggests that the Al in the monomeric AlCl<sub>4</sub><sup>-</sup> species is symmetrically coordinated to four Cl<sup>-</sup> ions with identical Al–Cl bond lengths (~2.16 Å). The Cl–Al–Cl bond angles (109.3°–109.7°) were close to the ideal tetrahedral bond angles (~109.5°). In the dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>, on the other hand, the coordination structure around Al is not symmetric. The Al-Cl bond length for six terminal Cl<sup>-</sup> ions is ~2.12 Å, while the Al-Cl bond length for the bridging Cl<sup>-</sup> is ~2.29 Å (denoted as Cl<sub>bridge</sub>). In addition, the Cl-Al-Cl bond angles in Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> vary between  $102^{\circ} - 114^{\circ}$ , further showing the distorted tetrahedral symmetry in the dimer. The TDDFT-simulated X-ray absorption spectra of monomeric AlCl4<sup>-</sup> and dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> species are presented in Supplementary Fig. 1. The theoretical spectra confirm that the increase in the pre-edge feature and the corresponding decrease in white line can be attributed to the systematic formation of dimeric  $Al_2Cl_7^-$  species within ionic liquids with higher  $AlCl_3/[C_4Py]Cl_3$ molar ratio.

Supplementary Fig. 2c shows the k<sup>2</sup>-weighted Fourier-transformed extended X-ray absorption fine structure (FT-EXAFS) of  $[C_4Py]Cl$ -xAlCl<sub>3</sub> ionic liquids with varying  $[C_4Py]Cl$ :AlCl<sub>3</sub> molar ratios. The FT-EXAFS shows a distinct feature at ~1.7 Å (phase-uncorrected) corresponding to Al–Cl scattering. A systematic broadening of this feature with increasing  $[C_4Py]Cl$ :AlCl<sub>3</sub> molar ratio suggests an increase in the Debye-Waller factor. A low Debye-Waller factor for ILs with  $[C_4Py]Cl$ :AlCl<sub>3</sub> = 1:1 is attributed to symmetric Al–Cl distances for all coordinated Cl atoms. On the other hand, in the dimeric Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> species, the larger Al–Cl<sub>bridge</sub> distance for the bridging Al atom

would contribute to an increase in the Debye-Waller factor and, thus, broadening of the Al–Cl scattering feature. This systematic increase in the Debye-Waller factor was also quantified by performing EXAFS fitting analysis (detailed fitting analysis is presented in Supplementary Figs. 3-6 and Supplementary Table 1). The fitting was performed using one Al–Cl single-scattering path obtained from the AlCl<sub>3</sub> crystal structure. The Al–Cl coordination number was fixed (= 4) during the fit. Supplementary Fig. 2d shows the fitted interatomic distances ( $R_{Al-Cl}$ ) and Debye-Waller factors ( $\sigma^2$ ) as a function of [C<sub>4</sub>Py]Cl:AlCl<sub>3</sub> molar ratios. In agreement with the following NMR and Raman analysis in Fig. 2, the systematic increase in the Debye-Waller factor supports a systematic conversion of monomers to dimers as the [C<sub>4</sub>Py]Cl:AlCl<sub>3</sub> ratio is increased from 1:1 to 1:2.



**Supplementary Fig. 2** | The X-ray absorption spectroscopy and quantitative evaluation of chloroaluminate species in ionic liquids. **a**, Al K-edge XANES of  $[C_4Py]Cl$ -*x*AlCl<sub>3</sub> ionic liquids (*x*=1-2). **b**, B3LYP/def2-TZVP-optimized structures of AlCl<sub>4</sub><sup>-</sup> and Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> ions. **c**, the k<sup>2</sup>-weighted Fourier-transformed extended X-ray absorption fine structure (FT-EXAFS) of  $[C_4Py]Cl$ -*x*AlCl<sub>3</sub> ionic

liquids (x=1-2). **d**, B3LYP/def2-TZVP-simulated Al K-edge X-ray absorption spectra of AlCl<sub>4</sub><sup>-</sup> and Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> anions. (Note: The experimentally obtained XANES of [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub> ionic liquids with AlCl<sub>3</sub>:[C<sub>4</sub>Py]Cl equal to 1:1 and 1:2, respectively, are also shown for comparison. The simulated spectra were energy-shifted by 27.1 eV).

Supplementary Table 1. Fitting parameters for the EXAFS of [C4Py]Cl-xAlCl<sub>3</sub> ionic liquids with varying AlCl<sub>3</sub>:[C4Py]Cl molar ratios. Fitting was performed in k-space simultaneously on the k<sup>1</sup>-, k<sup>2</sup>-, and k<sup>3</sup>-weighted data in the k-range between k = 2.7 Å<sup>-1</sup> and k = 8.0 Å<sup>-1</sup>. The Al–Cl coordination number was fixed (= 4.0) during the fitting.

		Al-Cl			D factor
AlCl <sub>3</sub> :[C <sub>4</sub> Py]Cl	$\Delta E_0 / eV$	CN <sup>a</sup>	<i>d</i> /Å	$\sigma^2  imes 10^3/\text{\AA}^2$	
1:1.0	$0.90\pm3.21$	4.0	$2.126\pm0.021$	$0.98 \pm 1.26$	0.043
1:1.3	$0.85\pm2.82$	4.0	$2.123\pm0.020$	$3.27 \pm 1.24$	0.044
1:1.4	$0.67\pm2.77$	4.0	$2.121\pm0.019$	$3.37 \pm 1.21$	0.041
1:1.5	$0.03\pm2.10$	4.0	$2.116\pm0.014$	$3.76 \pm 0.87$	0.048
1:1.6	$0.28\pm3.16$	4.0	$2.118\pm0.022$	$4.51 \pm 1.45$	0.051
1:1.7	$\textbf{-0.17} \pm 3.29$	4.0	$2.114\pm0.023$	$4.54 \pm 1.49$	0.057
1:1.8	$\textbf{-0.41} \pm \textbf{3.43}$	4.0	$2.111\pm0.024$	$5.12 \pm 1.59$	0.060
1:1.9	$\textbf{-0.36} \pm \textbf{3.63}$	4.0	$2.112\pm0.026$	$5.04 \pm 1.68$	0.060
1:2.0	$\textbf{-0.27} \pm 3.27$	4.0	$2.113\pm0.024$	$5.52 \pm 1.55$	0.053

<sup>a</sup>This parameter was fixed during the fit.



**Supplementary Fig. 3** | The corresponding Al–Cl coordination numbers and interatomic distances obtained from EXAFS fit.



**Supplementary Fig. 4** | Al K-edge EXAFS of  $[C_4Py]Cl$ -xAlCl<sub>3</sub> ionic liquids (x=1, 1.3, and 1.4), where the plots on the left-hand side show the  $k^2$ -weighted EXAFS and the plots on the right-hand side show the magnitude (green line) and the imaginary part (orange dots) of the Fourier transform spectra. Experimental data are shown as closed symbols, and the corresponding fits are shown as solid lines. (a)  $[C_4Py]Cl:AlCl_3 = 1:1$ , (b)  $[C_4Py]Cl:AlCl_3 = 1:1.3$ , and (c)  $[C_4Py]Cl:AlCl_3 = 1:1.4$ .



**Supplementary Fig. 5** | Al K-edge EXAFS of  $[C_4Py]Cl$ -xAlCl<sub>3</sub> ionic liquids (x=1.5, 1.6, and 1.7), where the plots on the left-hand side show the  $k^2$ -weighted EXAFS and the plots on the right-hand side show the magnitude (green line) and the imaginary part (orange dots) of the Fourier transform spectra. Experimental data are shown as closed symbols, and the corresponding fits are shown as solid lines. (a)  $[C_4Py]Cl:AlCl_3 = 1:1.5$ , (b)  $[C_4Py]Cl:AlCl_3 = 1:1.6$ , and (c)  $[C_4Py]Cl:AlCl_3 = 1:1.7$ .



**Supplementary Fig. 6** | Al K-edge EXAFS of  $[C_4Py]Cl$ -xAlCl<sub>3</sub> ionic liquids (x=1.8, 1.9, and 2.0), where the plots on the left-hand side show the  $k^2$ -weighted EXAFS and the plots on the right-hand side show the magnitude (green line) and the imaginary part (orange dots) of the Fourier transform spectra. Experimental data are shown as closed symbols, and the corresponding fits are shown as solid lines. (a)  $[C_4Py]Cl:AlCl_3 = 1:1.8$ , (b)  $[C_4Py]Cl:AlCl_3 = 1:1.9$ , and (c)  $[C_4Py]Cl:AlCl_3 = 1:2.0$ .



**Supplementary Fig. 7** | Temperature-programmed <sup>27</sup>Al MAS NMR spectroscopy on chloroaluminate ionic liquids. **a-f**, <sup>27</sup>Al MAS NMR spectra of  $[C_4Py]Cl-xAlCl_3$  (*x*=1-2.5) recorded during temperature-programmed process from 30 °C to 80 °C.



 $[C_4 Py]Cl\text{-}1AlCl_3$ 

 $\delta_{obs}$  = 443.84 -  $\delta_{calc}$  (443.84) + 103.0 ppm =103 ppm



[C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>

 $\delta_{\rm obs}$  (AI) = 443.84 -  $\delta_{\rm calc}$  (445.31) + 103.0 ppm =101.53 ppm

 $\delta_{obs}$  (AI) = 443.84 -  $\delta_{calc}$  (445.60) + 103.0 ppm =101.24 ppm



**Supplementary Fig. 8** | DFT-NMR modeling of  $Al_2Cl_7^-$  showing a broadened linewidth in the <sup>27</sup>Al MAS NMR spectra. **a**, DFT-NMR modeling of  $[C_4Py]Cl_1AlCl_3$  and set as reference at 103 ppm. **b**, DFT-NMR modeling of  $[C_4Py]Cl_2AlCl_3$  with calculated chemical shift of two Al nuclei. This result highlights the <sup>27</sup>Al chemicals shift of  $Al_2Cl_7^-$  can be merged into the peak located at around 103 ppm and is upfield shifted by about 2 ppm, thus causing a broadening of the peak at 103 ppm. **c**, Dynamic interconversion between  $Al_2Cl_7^-$  and  $AlCl_4^-$  via the transient reflected by the integrated linewidths quantified by the full width at half maximum (FWHM).



**Supplementary Fig. 9** | Raman spectra of [C<sub>4</sub>Py]Cl-*x*AlCl<sub>3</sub> (*x*=1-2).

# Supplementary Note 2: Derivations of concentration of AlCl₄<sup>-</sup> and Al<sub>2</sub>Cl<sub>7<sup>-</sup></sub> (Al<sub>2</sub>Cl<sub>7<sup>-</sup></sub>→ AlCl₄<sup>-</sup> + AlCl<sub>3</sub>) over various time intervals (t)

The chloroaluminate ionic liquids are synthesized by mixing anhydrous aluminium chloride with N-butylpyridinium chloride at various ratios, denoted as  $[C_4Py]Cl-xAlCl_3$  ( $x \in [1,2]$ ). The formation of  $[C_4Py]Cl-xAlCl_3$  can simplify as:

$$[C_4Py]Cl + xAlCl_3 \rightarrow [C_4Py]^{\oplus} + (x-1)Al_2Cl_7^{\ominus} + (2-x)AlCl_4^{\ominus}$$
 [Rxn S1]

The dissociation of  $Al_2Cl_7^{\ominus}$  further generates  $AlCl_4^{\ominus}$  and  $AlCl_3$ -adduct:

$$Al_2Cl_7^{\ominus} \rightarrow AlCl_4^{\ominus} + AlCl_3...adduct$$
 [Rxn S2]

Letting the overall concentrations of AlCl<sub>3</sub>...adduct be  $\sum$ [AlCl<sub>3</sub>...adduct], then we have:

$$\Delta[AlCl_4^{\ominus}] = \sum [AlCl_3 \cdots adduct]$$
 (Eq. S1)

The changes of concentration of  $[Al_2Cl_7^{\ominus}]_t$ ,  $[AlCl_4^{\ominus}]_t$  and  $\sum [AlCl_3 \cdots adduct]_t$  at different times can be expressed as:

$$\Delta \left[Al_2 C l_7^{\ominus}\right]_t = \left[Al_2 C l_7^{\ominus}\right]_0 - \left[Al_2 C l_7^{\ominus}\right]_t$$
(Eq. S2)

$$\Delta [AlCl_4^{\ominus}]_t = \sum [AlCl_3 \cdots adduct]_t = [AlCl_4^{\ominus}]_0 + [AlCl_4^{\ominus}]_t$$
(Eq.S3)

$$\frac{[Al_2Cl_7^{\ominus}]_0}{[AlCl_4^{\ominus}]_0} = \frac{x-1}{2-x}$$
(Eq. S4)

$$\frac{[Al_2Cl_7^{\ominus}]_t}{[AlCl_4^{\ominus}]_t} = \frac{[Al_2Cl_7^{\ominus}]_0 - \sum [AlCl_3 \cdots adduct]_t}{[AlCl_4^{\ominus}]_0 + \sum [AlCl_3 \cdots adduct]_t}$$
(Eq. S5)

By substituting with equations S1-S5, the initial concentration of  $[C_4Py]Cl-xAlCl_3$  was denoted as  $n_0$  mol, then we have:

$$\frac{[Al_2Cl_7^{\ominus}]_t}{[AlCl_4^{\ominus}]_t} = \frac{(x-1)n_0 - \sum [AlCl_3 \cdots adduct]_t}{(2-x)n_0 + \sum [AlCl_3 \cdots adduct]_t}$$
(Eq. S6)

The area ratio of Raman signals at 310 cm<sup>-1</sup> and 350 cm<sup>-1</sup> depends closely on the molar ratio of  $Al_2Cl_7^{\ominus}$  to  $AlCl_4^{\ominus 18-2018-2017-19}$ , showing a linear correlation with a constant  $k_{SCS}$ , the coefficient:

$$\frac{[Al_2Cl_7 \ominus]_t}{[AlCl_4 \ominus]_t} = k_{SCS} \left(\frac{Area_{310 \ cm^{-1}}}{Area_{350 \ cm^{-1}}}\right)_t$$
(Eq. S7)

From Fig. 2e in the main text showing that the  $\left(\frac{\text{Area}_{310 \text{ cm}^{-1}}}{\text{Area}_{350 \text{ cm}^{-1}} + \text{Area}_{310 \text{ cm}^{-1}}}\right)_0$  is proportional to x (x = the molar ratio of AlCl<sub>3</sub>/[C<sub>4</sub>Py]Cl), we have:

$$\left(\frac{Area_{310\ cm^{-1}}}{Area_{350\ cm^{-1}} + Area_{310\ cm^{-1}}}\right)_0 = 1.04x - 1.08 \qquad (R^2 = 0.994) \qquad (Eq. S8)$$

Based on equations S4, S7 and S8, the  $k_{SCS}$  and  $\sum [AlCl_3 \cdots adduct]_t$  can be expressed as:

$$k_{SCS} = \frac{(2.08 - 1.04x)(x - 1)}{(2 - x)(1.04x - 1.08)}$$
(Eq.S9)

$$\sum_{t} [AlCl_{3} \cdots adduct]_{t} = (x-2)n_{0} + \frac{n_{0}}{k_{SCS} \left(\frac{Area_{310 \ cm^{-1}}}{Area_{350 \ cm^{-1}}}\right)_{t} + 1}$$
(Eq. S10)

$$\left[AlCl_{4}^{\ominus}\right]_{t} = (2x - 4)n_{0} + \frac{n_{0}}{k_{SCS} \left(\frac{Area_{310 \ cm^{-1}}}{Area_{350 \ cm^{-1}}}\right)_{t} + 1}$$
(Eq. S11)

$$[Al_2Cl_7^{\ominus}]_t = n_0 - \frac{n_0}{k_{SCS} \left(\frac{Area_{310\ cm^{-1}}}{Area_{350\ cm^{-1}}}\right)_t} + 1$$
(Eq. S12)

The Al mole fraction  $(\chi_{Al})$  of chloroaluminate species can be expressed as:

$$\chi_{Al} (Al_2 C l_7^{\ominus})_t = \frac{2[A l_2 C l_7^{\ominus}]_t}{x n_0};$$

$$\chi_{Al} (A l C l_4^{\ominus})_t = \frac{[A l C l_4^{\ominus}]_t}{x n_0};$$

$$\chi_{Al} (\sum [A l C l_3 \cdots a d d u c t])_t = \frac{\sum [A l C l_3 \cdots a d d u c t]_t}{x n_0}$$
(Eq. S13)

We then plotted the  $k_{SCS}$  against x using equation S8, see below:



## ✤ For [C4Py]Cl-2AlCl3 (x=2)

 $\lim_{x\to 2} k_{SCS} = 1$ , the concentration of chloroaluminate species can be rewritten as:

$$\left[AlCl_{4}^{\ominus}\right]_{t} = \frac{n_{0}}{\left(\frac{Area_{310\ cm^{-1}}}{Area_{350\ cm^{-1}}}\right)_{t} + 1}$$
(Eq. S14)

$$[Al_2Cl_7^{\ominus}]_t = n_0 - \frac{n_0}{\left(\frac{Area_{310\ cm^{-1}}}{Area_{350\ cm^{-1}}}\right)_t} + 1$$
(Eq. S15)

The Al mole fraction  $(\chi_{Al})$  of chloroaluminate species can be expressed as:

$$\chi_{Al}(\Sigma[Al - adduct])_{t} = \chi_{Al}(AlCl_{4}^{\ominus})_{t} = \frac{1}{2\left(\frac{Area_{310\ cm^{-1}}}{Area_{350\ cm^{-1}}}\right)_{t} + 2}$$
(Eq. S16)

$$\chi_{Al} (Al_2 C l_7^{\ominus})_t = 1 - \frac{1}{\left(\frac{Area_{310 \ cm^{-1}}}{Area_{350 \ cm^{-1}}}\right)_t} + 1}$$
(Eq. S17)



**Supplementary Fig. 10** | The computational simulation of the dissociation of  $Al_2Cl_7^-$  in a DCM solvent. The standard Helmholtz free energies ( $\Delta F^\circ$ ) as a function of the Al distance between two Al center of  $Al_2Cl_7^-$  (These data were acquired through ab initio molecular dynamics simulations in conjunction with the Blue Moon ensemble method).



**Supplementary Fig. 11** | **a**, Illustration of chloroaluminate transformation in the presence of TBC The initial reaction rate as a function of TBC concentration . **b**, The initial LDPE conversion rate as a function of  $\frac{[Al_2Cl_7] \cdot [TBC]}{[AlCl_4]^*}$  concentration. The concentration of  $\frac{[Al_2Cl_7] \cdot [TBC]}{[AlCl_4]^*}$  was determined by varying the molar ratio of initial anhydrous AlCl<sub>3</sub> and [C<sub>4</sub>Py]Cl, and TBC amount. Note that: the initial rates calculated as grams of LDPE converted per hour and per mole of Al content. The concentration of AlCl<sub>3</sub>-adducts (AlCl<sub>3</sub>···Cl···C4) can be expressed as:  $[AlCl_3 \cdot \cdot Cl \cdot \cdot C4] = \frac{[Al_2Cl_7] \cdot [TBC]}{[AlCl_4] \cdot *K}$ . The plot of Log(r) *vs*. Log( $\frac{[Al_2Cl_7] \cdot [TBC]}{[AlCl_4]^*}$ ) showed a nearly follow first order kinetics. The initial reaction rate is directly proportional to the concentration of TBC loading.



**Supplementary Fig. 12** | Raman spectroscopy analysis of the interaction between TBC and  $[C_4Py]Cl-xAlCl_3$ . **a**, Raman spectra of neat  $[C_4Py]Cl-xAlCl_3$  ionic liquids. **b**. Raman spectra of  $[C_4Py]Cl-xAlCl_3$  ionic liquids in the presence of TBC. Spectra recorded at room temperature with TBC to  $[C_4Py]Cl-xAlCl_3$  molar ratio of 1/10. **c**. Plot of the Raman area ratio of  $Al_2Cl_7^-$  versus the molar ratio of  $AlCl_3/[C_4Py]Cl(x)$ .



**Supplementary Fig. 13** | The conversion of LDPE plotted against the corresponding variation of chloroaluminate species in ionic liquids. The corresponding data are derived from the Raman spectra in Fig. 4b in main text.



**Supplementary Fig. 14** | **a**, In situ Raman spectra recorded during the cracking-alkylation of n- $C_{16}H_{34}$  and i $C_5$  in the presence of TBC additive. **b**, The time-resolved conversion profile of n- $C_{16}H_{34}$  and the corresponding variation of chloroaluminate species in ionic liquids. Conditions were as follows: **a**-**b**: n- $C_{16}H_{34}$ , 200mg;  $iC_5$ , 800 mg;  $[C_4Py]Cl$ -2AlCl<sub>3</sub>, 2 mmol; TBC, 5 mg; DCM, 3 ml; and temperature, 70 °C.



**Supplementary Fig. 15** | The computational simulations of  $Al_2Cl_7^-$  catalyzed hydride abstraction from *i*C<sub>5</sub>. The standard Helmholtz free energies ( $\Delta F^\circ$ ) as a function of the Al–H distance ( $R_{Al-H}$ ) between two molecules, accompanied by atomic configurations that depict the initial and intermediate states. These data were derived through ab initio molecular dynamics simulations in conjunction with the Blue Moon ensemble method.



Supplementary Fig. 16 | Computational simulation of AlCl<sub>3</sub>-TBC adduct catalyzing hydride abstraction from nC<sub>16</sub>. The standard Helmholtz free energies ( $\Delta F^{\circ}$ ), dependent on the H–Cl distance (R<sub>H–Cl</sub>) between two molecules, are accompanied by atomic configurations that represent the initial, transition, and intermediate states. These data were acquired through ab initio molecular dynamics simulations in conjunction with the Blue Moon ensemble method.



**Supplementary Fig. 17** | In situ 1H NMR spectra of tandem cracking-alkylation of n-C<sub>16</sub> and iC<sub>5</sub> over [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>. **a**, The representative in situ <sup>1</sup>H NMR spectra varying n-C<sub>16</sub> and iC<sub>5</sub> loading. **b**, the fraction of total alkenes correlates with time. Conditions: Hexadecane (n-C<sub>16</sub>) 0.16 mmol, isopentane (*i*C<sub>5</sub>) 0-0.90 mmol, C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub> 0.23 mmol, TBC 0.5  $\mu$ mol, CD<sub>2</sub>Cl<sub>2</sub>, 25 °C, 4 h.

Note: For a typical experiment, an NMR tube was charged with  $[C_4PyCl]-2AlCl_3$  (0.23 mmol),  $C_{16}$  (0.16 mmol or 2.5 mmol C), and TBC (0.5 µmol). Varying amounts of iC<sub>5</sub> were added under the standard reaction conditions previously described to investigate the impact of the alkylating

agent on alkene detection. The variation in the number of unsaturated hydrogen atoms within the olefinic region (4.4–6.5 ppm). This variability indicates the presence and fluctuation of olefinic intermediates throughout the reaction. The ratio of unsaturated chains remains constant, maintaining a low concentration approximately between 0.2-0.5% throughout the reaction.



**Supplementary Fig. 18** | Raman spectroscopy analysis of the interaction between TBC and  $[C_4Py]Cl-2AlCl_3$ . **a**, Raman spectra of  $[C_4PyCl]-2AlCl_3$  ionic liquids in the presence of pentene  $(C_5^{-})$  and (b) The corresponding variation of chloroaluminate species. Note: spectra recorded at room temperature with varying  $C_5^{-}$  amount (0-0.2mmol) to 2 mmol  $[C_4PyCl]-2AlCl_3$  ionic liquids.

The spectra of  $[C_4Py]Cl-2AlCl_3$  remained virtually unchanged in the presence of varying concentrations of pentene ( $C_5^=$ ) as well as in its absence. This observation implies that olefin incorporation does not promote the dissociation of  $Al_2Cl_7^-$ .



**Supplementary Fig. 19** | Time-resolved conversion profile of LDPE in the presence of TBC or  $C_5^{=}$  as additives, compared to conditions without additives. Reaction conditions: LDPE 200 mg, *i*C<sub>5</sub> 800 mg, [C<sub>4</sub>Py]Cl-AlCl<sub>3</sub> 3 mmol, additive 0.05 mmol, DCM 3 mL, 70 °C.

Note: the introduction of  $C_5^=$  gave only 18 wt.% conversion to LDPE, exhibiting no discernible enhancement when compared to the baseline conditions that lacked such additives. In contrast, the addition of TBC significantly increased the initial reaction rate, resulting in 100% of LDPE conversion within 180 mins (3h). Obviously,  $C_5^=$  exhibits a pronounced preference for alkylation with i.



Supplementary Fig. 20 | Computed reaction pathway for the formation of AlCl<sub>3</sub>-C<sub>5</sub><sup>=</sup> adduct. Plotted is the standard Helmholtz free energy ( $\Delta F^{\circ}$ ) as a function of the internuclear distance of Al-H for the reaction of Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> and C<sub>5</sub><sup>=</sup> to form AlCl<sub>4</sub><sup>-</sup> and a AlCl<sub>3</sub>-C<sub>5</sub><sup>=</sup> adduct.  $\Delta F^{\circ}$  is calculated using the Blue Moon ensemble approach for ab initio molecular dynamics. Included are representative structures along the reaction pathway.



**Supplementary Fig. 21** | **a**, Photograph of the Operando IR setup combing a ReactIRTM 45m spectrometer connected to a 150 mL Parr autoclave, with a probe window connected to the sentinel probe through the conduit K4 (Photo: W. Zhang/ Lercher's Lab in TU Munich). **b**, Schematic illustration of the corresponding Operando IR setup and autoclave reactor.



**Supplementary Fig. 22** | Operando IR spectra were recorded during LDPE depolymerization in the absence of iC<sub>5</sub> over ionic liquids ([C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>). **a**, The time-resolved full spectra, Data were acquired with an automatic sample scan interval of 15s over the range of 3200-650 cm<sup>-1</sup>, and only presented the selected data with an interval of 5 min. **b**, Three-dimensional spectra of the *sp*<sup>3</sup> C–H vibrations. **c**, the selected IR spectra were recorded during LDPE depolymerization in the presence of *i*C<sub>5</sub> over ionic liquids ([C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>) at 1, 2, 30, 60 and 120 min. Conditions were as follows: LDPE, 2 g; DCM, 30 ml; [C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>, 20 mmol; TBC 0.5 mmol, and temperature, 60 °C.



**Supplementary Fig. 23** | Three-dimensional operando IR spectra of the  $sp^3$  C–H vibrations as a function of reaction time, recorded during LDPE depolymerization in the presence of iC<sub>5</sub> over ionic liquids ([C<sub>4</sub>Py]Cl-2AlCl<sub>3</sub>) at 60 °C. The corresponding full spectra are shown in Fig. 5 in the main text.



Supplementary Fig. 24 | Reference IR spectra of pure compounds including isopentane (iC<sub>5</sub>), Dichloromethane (DCM), 1-pentene ( $C_5^=$ ) and [ $C_4Py$ ]Cl-2AlCl<sub>3</sub> in DCM, respectively.



Supplementary Fig. 25 | Operando IR spectra of the iC<sub>5</sub> on-off experiment. Conditions were as follows: LDPE, 2 g;  $iC_5$ , 8 g;  $[C_4Py]Cl-2AlCl_3$ , 20 mmol; and temperature, 60 °C. Data were acquired with an automatic sample scan interval of 15s over the range of 4000-700 cm<sup>-1</sup>.

Supplementary Note 3: Derivations of rate equations in the cracking-alkylation of polyolefin with *i*C<sub>5</sub> over [C<sub>4</sub>Py]Cl-*x*AlCl<sub>3</sub>



Supplementary Fig. 26 | Proposed sequence of key reaction steps in the cracking-alkylation of polyolefin with iC<sub>5</sub> over [C<sub>4</sub>Py]Cl-xAlCl<sub>3</sub>. All resulting carbenium ion-intermediates are not bare species but surrounded and stabilized by the counterpart  $AlCl_4^-$  to form ion pairs (see details in Fig. 6 in the main text).

We propose a set of key elementary steps (shown in Fig. 6 and Supplementary Fig. 26) that involves three main stages of carbenium ions-mediated mechanism: initial formation of carbenium ions via chloride and hydride transfer, propagation of cracking and alkylation cycles of carbenium ions, and termination of carbenium ions. The overall reaction is started by small amounts of TBC reacting with AlCl<sub>3</sub> species that are in situ generated from the dissociating Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup>, providing the initial carbenium ions to start the chain process. Then, AlCl<sub>4</sub><sup>-</sup>-coordinated carbenium ions act as reactive ion-pair intermediates that activate the C–H bonds of hydrocarbons (either LDPE or  $iC_5$ ), followed by C–H bond cleavage via hydride transfer to preferentially form tert-carbenium ions in the polymer and in the more abundant  $iC_5$ .

Next, the formed polyolefin carbenium ion-pairs undergo isomerization and cracking via  $\beta$ -scission, which yields short carbenium ions and alkenes. Simultaneously, the formed alkenes reacted with *i*C<sub>5</sub> via the alkylation step, shifting the equilibrium and catalyzing polyolefin

conversion. The long-chain fragments undergo further cracking, and alkylation cycles to the branched alkylate. Finally, the carbenium- $AlCl_4^-$  ion-pairs can be terminated either by deprotonation to an alkene followed by oligomerization (without replenishing of *i*C<sub>5</sub>), or by recombination of hydride or chloride, i.e., the reverse of the initiation reaction (without replenishing of polyolefin) that  $Al_2Cl_7^-$  regenerated again reacts with  $AlCl_4^-$  to  $Al_2Cl_7^-$ .

Letting the overall concentrations of AlCl<sub>3</sub>...adduct be  $\sum$ [AlCl<sub>3</sub>...adduct], then we have:

$$\Delta[Al_2Cl_7^{\ominus}] = \Delta[AlCl_4^{\ominus}] = \sum [AlCl_3 \cdots adduct]$$

The proposed sequence of key reaction steps in the cracking-alkylation of polyolefin with  $iC_5$  can be simplified as follows:

$$C_nH_{2n+2} + AlCl_3...adduct$$
  $(Rxn S1)$ 

$$iC_5H_{12}$$
 +AICI<sub>3</sub>...adduct  $= \frac{1}{\sqrt{2}}iC_5H_{11}...H...AICI_3...adduct$  (Rxn S2)

$$C_{n}H_{2n+1}...H...AICI_{3}...adduct \qquad \stackrel{\frown}{\leftarrow} C_{n}H_{2n+1} + \{AICI_{3}...adduct...H\}^{\bigcirc}$$
(Rxn S3)

$$K_{H2}$$
  $\bigcirc$   
 $iC_5H_{11}...H...AlCl_3...adduct  $\xrightarrow{\oplus}$   $iC_5H_{11}$  + {AlCl_3...adduct...H}  $\bigcirc$  (Rxn S4)$ 

$$\bigoplus_{n \in \mathbb{Z}_{n+1}}^{\textcircled{\text{C}}} + \{A|C|_3...adduct...H\} \bigoplus_{k_{oligom}}^{\textcircled{\text{C}}} C_x H_{2x}^{=} + C_{n-x} H_{2(n-x)+1}^{\textcircled{\text{C}}} + \{A|C|_3...adduct...H\} \bigoplus_{k=1}^{\textcircled{\text{C}}} (Rxn S5)$$

$$C_{x}H_{2x}^{=} + iC_{5}H_{11}^{\oplus} + \{A|C|_{3}...adduct...H\} \xrightarrow{\bigcirc} k_{a|ky|} C_{x+5}H_{2x+12} + A|C|_{3}...adduct \qquad (Rxn S6)$$

 $AICI_3...adduct \longrightarrow C_i^{\circ} + AICI_4^{\circ}$   $AICI_3...adduct...H)^{\circ} \longrightarrow C_i + AICI_4^{\circ}$ 

where active AlCl<sub>3</sub>-adducts with PE and  $iC_5$  (Rxn S1-S2) and the subsequent C–H bond cleavages (Rxn S3-S4) are proposed to be rapid and quasi-equilibrated, K<sub>a1</sub>, K<sub>a2</sub>, K<sub>H1</sub> and K<sub>H2</sub> are the reaction equilibrium constant, respectively. We have:

$$K_{a1} = \frac{\left[C_n H_{2n+1} \cdots H \cdots AlCl_3 \cdots adduct\right]}{\left[C_n H_{2n+2}\right] \left[AlCl_3 \cdots adduct\right]}$$
(Eq. S1)  
$$K_{a2} = \frac{\left[iC_5 H_{11} \cdots H \cdots AlCl_3 \cdots adduct\right]}{\left[C_n H_{2n+2}\right] \left[AlCl_3 \cdots adduct\right]}$$
(Eq. S2)

$$\kappa_{a2} = \frac{[iC_5H_{12}][AlCl_3 \cdots adduct]}{[iC_5H_{12}][AlCl_3 \cdots adduct]}$$
(Eq. 5)

$$K_{H1} = \frac{\left[C_n H_{2n+1}^{-1}\right]\left[AlCl_3 \cdots adduct \cdots H\right]^{\ominus}\right]}{\left[C_n H_{2n+1} \cdots H \cdots AlCl_3 \cdots adduct\right]}$$
(Eq. S3)  
$$\left[iC_5 H_{11}^{\oplus}\right]\left[AlCl_3 \cdots adduct \cdots H\right]^{\ominus}\right]$$

$$K_{H2} = \frac{[lc_5H_{11}][Hcl_3 \cdots uuuucl \cdots H_3^{+}]}{[iC_5H_{11} \cdots H \cdots AlCl_3^{+}]}$$
(Eq. S4)

We reasoned that cracking and alkylation occurred simultaneously and proceeded constantly. Because the activated hydrocarbon strands of polymers will crack at positions that are determined by the rates of hydride shift within the chain. Increasing the hydride shift rate compared to cracking will lead to longer cracked fragments and heavier products; on the contrary, the relatively higher rate of cracking will give more alkenes, facilitating the formation of acid-soluble oil via oligomerization (as the alkylation is a significantly slower reaction than the oligomerization of the alkenes). Thus, the initial reaction rate (r) can be expressed as:

$$r = k_{crack} [C_n H_{2n+1}^{\oplus}] [AlCl_3 \cdots adduct \cdots H]^{\ominus}]$$
  
-  $k_{oligom} [C_{n-x} H_{2(n-x)+1}^{\oplus}] [AlCl_3 \cdots adduct \cdots H]^{\ominus}] [C_x H_{2x}^{=}]$   
=  $k_{alkyl} [iC_5 H_{11}^{\oplus}] [AlCl_3 \cdots adduct \cdots H]^{\ominus}] [C_x H_{2x}^{=}]$   
(Eq. S5)

Note that the long-chain fragments  $(C_{n-x})$  underwent further cracking and alkylation cycles. The rates of both associations of AlCl<sub>3</sub>-adducts with  $C_{n-x}$  and the subsequent C–H bond cleavages were identical to that Rxn S1 and Rxn S3, then we have

$$K_{a1} = \frac{\left[C_{n-x}H_{2(n-x)+1}\cdots H\cdots AlCl_{3}\cdots adduct\right]}{\left[C_{n-x}H_{2(n-x)+2}\right]\left[AlCl_{3}\cdots adduct\right]}$$
(Eq. S6)

$$K_{H1} = \frac{\left[C_{n-x}H_{2(n-x)+1}^{\oplus}\right]\left[AlCl_{3}\cdots adduct\cdots H\}^{\ominus}\right]}{\left[C_{n-x}H_{2(n-x)+1}\cdots H\cdots AlCl_{3}\cdots adduct\right]}$$
(Eq. S7)

Combing Equations S1-S4 and S6-7, gives:

$$[C_{x}H_{2x}^{=}] = \frac{k_{crack}K_{H1}K_{a1}[C_{n}H_{2n+2}]}{k_{alkyl}K_{H2}K_{a2}[iC_{5}H_{12}] + k_{oligom}K_{H1}K_{a1}[C_{n-x}H_{2(n-x)+2}]}$$
(Eq. S8)

We assumed that in the kinetic regime, the concentration of  $C_nH_{2n+2}$  is identical to  $C_{n-x}H_{2(n-x)+2}$ , then we have

$$[C_x H_{2x}^{=}] = \frac{k_{crack} K_{H1} K_{a1} [C_n H_{2n+2}]}{k_{alkyl} K_{H2} K_{a2} [iC_5 H_{12}] + k_{oligom} K_{H1} K_{a1} [C_n H_{2n+2}]}$$
(Eq. S9)

Overall, Taking Equation S7 to Equation S5, the rate equation can be expressed as:

$$r = k_{alkyl} [iC_{5}H_{11}^{\oplus}] [AlCl_{3} \cdots adduct \cdots H]^{\ominus} ] [C_{x}H_{2x}^{=}]$$

$$= \frac{k_{alkyl}k_{crack}K_{H1}K_{H2}K_{a1}K_{a2}[C_{n}H_{2n+2}][iC_{5}H_{12}]}{k_{alkyl}K_{H2}K_{a2}[iC_{5}H_{12}] + k_{oligom}K_{H1}K_{a1}[C_{n}H_{2n+2}]} [AlCl_{3} \cdots adduct]$$

$$= \frac{k_{alkyl}k_{crack}K_{H1}K_{H2}K_{a1}K_{a2}[C_{n}H_{2n+2}][iC_{5}H_{12}]}{k_{alkyl}K_{H2}K_{a2}[iC_{5}H_{12}] + k_{oligom}K_{H1}K_{a1}[C_{n}H_{2n+2}]} [AlCl_{3}]_{total} \quad (Eq. S10)$$

The rate normalized to the total AlCl<sub>3</sub> concentration (r<sub>Al</sub>) can be expressed as:

$$r_{Al} = \frac{1}{\sum [AlCl_3 - adduct]} = \frac{k_{alkyl}k_{crack}K_{H1}K_{H2}K_{a1}K_{a2}[C_nH_{2n+2}][iC_5H_{12}]}{k_{alkyl}K_{H2}K_{a2}[iC_5H_{12}] + k_{oligom}K_{H1}K_{a1}[C_nH_{2n+2}]}$$
(Eq. S11)



**Supplementary Fig. 27** | Kinetic analysis of cracking-alkylation cycles of polyolefin with iC<sub>5</sub>. **a-c**, Regression of the  $r_{A1}$  with concentrations of polyolefin [C<sub>n</sub>H<sub>2n+2</sub>], [C<sub>16</sub>] and isopentane [*i*C<sub>5</sub>H<sub>12</sub>], respectively, showing excellent fits to equation (Eq. (3)) in the main text.